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Microporous Acidic Cesium Salt of 12-Tungstosilicic Acid $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ as a Size-selective Solid Acid Catalyst

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An acidic Cs salt of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ ($\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$), which was prepared by titrating an aqueous solution of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ with an aqueous solution of Cs_2CO_3 , possessed only micropores and exhibited size-selective catalysis for acid-catalyzed reactions in liquid phase.

Crystalline microporous oxides, such as zeolites, are useful materials for various applications, including catalysts, ion-exchange materials, adsorbents, and molecular sieves.¹ In catalysis, microporous oxides are able to act as size-selective catalysts due to their constrained pore size, and zeolites are typical examples of size-selective solid acid catalysts.²⁻⁴ However, their applications are limited because the acid strengths are relatively weak. Thus, a variety of microporous oxides other than zeolites have been synthesized for potential use as solid acid catalysts.⁵⁻⁹

Heteropoly acids are oxide clusters with well-defined basic structures. They are fascinating and important catalysts from a practical standpoint because they are strong acids and are much more active than zeolites, such as H-ZSM-5, in various acid catalyzed reactions.¹⁰⁻¹³ Among heteropoly acids, the Keggin-type heteropoly acid $\text{H}_3\text{PW}_{12}\text{O}_{40}$ and its acidic Cs salts have been extensively studied because of their high stability, strong acidity, and high surface area.^{10,11,14} It has been reported that $\text{Cs}_{2.1}\text{H}_{0.9}\text{PW}_{12}\text{O}_{40}$ (abbreviated as Cs2.1-P) is microporous¹⁵⁻¹⁷ and that this acts as a size-selective catalyst for acid-catalyzed reactions.¹⁵ In addition, its platinum-modified form shows size-selective catalytic activity towards the hydrogenation of alkenes and the complete oxidation of alkanes.¹⁸

In contrast, there are only a few reports involving Cs salts of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$, though $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ is a Keggin-type heteropoly acid similar to $\text{H}_3\text{PW}_{12}\text{O}_{40}$. Moffat et al.¹⁹ have reported that a neutral Cs salt of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$, $\text{Cs}_4\text{SiW}_{12}\text{O}_{40}$, is microporous with a high surface area ($150 \text{ m}^2 \text{ g}^{-1}$), but the size of its micropores is uncertain. Blanco and coworkers have reported a synthesis of acidic Cs salts of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$, $\text{Cs}_{3.4}\text{H}_{0.6}\text{SiW}_{12}\text{O}_{40}$ and $\text{Cs}_{3.8}\text{H}_{0.2}\text{SiW}_{12}\text{O}_{40}$, and their acid catalytic activity towards phenol tetrahydropyranlation.²⁰ However, the salts that they prepared have mesopores as well as micropores, and thus, size-selective catalytic reactions over them have not been attempted. In this study, we synthesized microporous $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ with little mesopores and a high surface area. Here we report that $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ exhibits size-selective catalytic activity towards acid catalyzed reactions in a liquid-solid reaction system. Since the formation mechanism of the micropores in $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ is completely different from that in Cs2.1-P (discussed later), the pore sizes are different between the two, leading to different size-selective catalytic properties.

We prepared acidic Cs salts, $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, by titrating an aqueous solution of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ (0.08 mol dm^{-3}) with an aqueous solution of Cs_2CO_3 (0.10 mol dm^{-3}). In the preparation, the addition of aqueous Cs_2CO_3 solution was carefully controlled by using an automatic syringe pump: first, 2 cm^3 was added at a rate of $0.033 \text{ cm}^3 \text{ min}^{-1}$, and then the remaining solution was added at a rate of $0.2 \text{ cm}^3 \text{ min}^{-1}$. The resulting colloidal solution was allowed to stand for 48 h at room temperature and then evaporated to obtain $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ as a white solid. If one added the aqueous Cs_2CO_3 solution to the aqueous solution of $\text{H}_4\text{SiW}_{12}\text{O}_{40}$ at a constant rate of $0.2 \text{ cm}^3 \text{ min}^{-1}$ from the beginning of the titration, fine particles with large external surface area were formed, which had adverse effects in the size selective catalysis. Thus, the careful control of the addition of the aqueous Cs_2CO_3 solution is very important.

Catalytic reactions (Figure S1²¹) were performed in a three-neck flask (100 cm^3) after the catalysts were pretreated in a He flow at 473 K for 0.5 h. The reactions were carried out using isopropyl acetate (8 mmol) in *n*-decane (140 mmol) at 373 K, cyclohexyl acetate (14 mmol) in *n*-nonane (112 mmol) at 343 K, *tert*-butyl acetate (20 mmol) in *n*-decane (125 mmol) at 313 K, α -pinene (0.64 mmol) in toluene (97 mmol) at 273 K, and cyclohexane (10 mmol) in 1,3,5-trimethylbenzene (216 mmol) at 363 K.

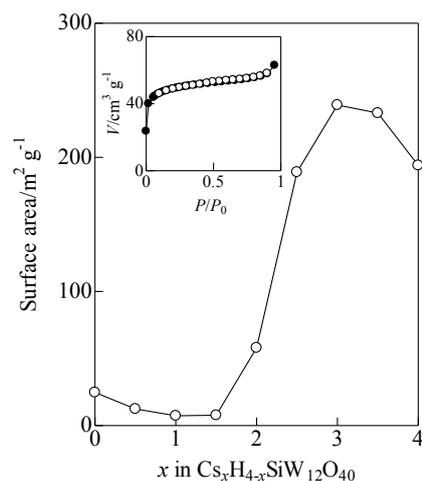


Figure 1. Surface area of $\text{Cs}_x\text{H}_{4-x}\text{SiW}_{12}\text{O}_{40}$. The surface area was determined from an N_2 adsorption isotherm at 77 K after pretreatment of the catalyst at 473 K in a flow of N_2 . Inset: N_2 adsorption and desorption isotherm for $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ at 77 K.

As shown in Figure 1, the changes in the surface area as a function of Cs content in $\text{Cs}_x\text{H}_{4-x}\text{SiW}_{12}\text{O}_{40}$ were remarkable. The surface areas were estimated on the basis of a Langmuir plot obtained from an N_2 adsorption isotherm at 77 K because all of the Cs salts were microporous. The surface area increased significantly when the Cs content (x) exceeded 1.5 and reached maximum at $x = 3$ ($239 \text{ m}^2 \text{ g}^{-1}$), although it decreased slightly when $x > 3$.

As shown in the inset of Figure 1, $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ which had the highest surface area gave a type I isotherm of N_2 adsorption-desorption at 77 K, indicating that this material was microporous. The total and external surface area were estimated from the slopes of two lines in a t -plot to be $191 \text{ m}^2 \text{ g}^{-1}$ and $7 \text{ m}^2 \text{ g}^{-1}$, respectively (Figure S2¹). The external surface area corresponded to less than 4% of the total surface area.

In order to determine the micropore size distribution of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, we acquired an Ar adsorption isotherm at 87 K. Figure 2 shows pore-size distributions of the micropores as well as mesopores of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$. The micropore and mesopore size distributions were determined from the Ar adsorption isotherm by using the Saito-Foley method²² and from an N_2 adsorption isotherm by using the Dollimore-Heal method,²³ respectively. As a reference, micropore-size distribution of Cs2.1-*P* is put in the figure. In the micropore-size distribution for $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, an intense peak at 0.53 nm and a shoulder at around 0.69 nm were observed. On the other hand, only a small amount of the mesopores was present.

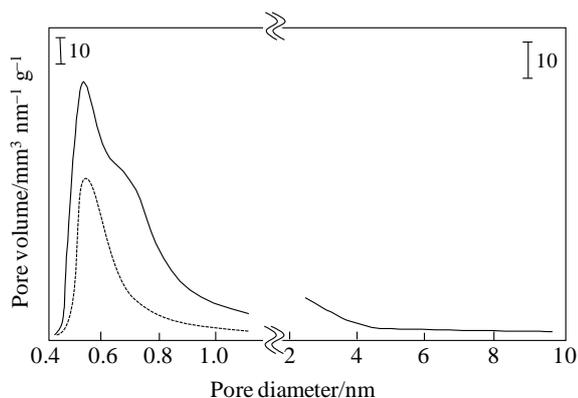


Figure 2. Micropore and mesopore size distributions for $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ (solid line) and micropore size distribution for Cs2.1-*P* (dotted line). Micropore size distribution was determined by using the Saito-Foley method on an Ar adsorption isotherm, and mesopore size distribution was determined by using the Dollimore-Heal method on an N_2 desorption isotherm.

The peak position for Cs2.1-*P* was similar to that for $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, but the pore-size distribution was narrow and the larger-size micropores were nonexistent in it.

The size of the crystallites of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ was estimated to be about 49 nm from the linewidth in the X-ray diffraction (XRD) pattern. Assuming the external surface is only the surface of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, the surface area was calculated from the density and the particle size to be $19 \text{ m}^2 \text{ g}^{-1}$. However, this value was significantly smaller than the actual surface area ($239 \text{ m}^2 \text{ g}^{-1}$). This great difference can be explained if micropores are present inside the crystallites of

$\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$. $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ showed a XRD pattern due to body-centered cubic (BCC) structure (Figure S3²¹), in which the locations of heteropoly anion ($\text{SiW}_{12}\text{O}_{40}^{4-}$) are allowable in the center and each corner of the unit cell, and that of Cs^+ or H^+ is between two heteropoly anions. To construct the BCC structure, heteropoly anions to cations (Cs^+ and H^+) ratio must be one third, while the actual ratio was one fourth due to the charge balance. Thus it would be expected that quarter heteropoly anions were defective, in other words, anion vacancies were present in the crystallites. Therefore, these anion vacancies formed the micropores of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$. In contrast to $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$, the crystallites of Cs2.1-*P* were nonporous.¹⁶ Thus its micropores are considered to be interparticle voids between the crystallites. The difference in the formation mechanism of the micropores results in micropore sizes between the two, though the size of heteropoly anions are very similar each other. Schlögl and coworkers have proposed a similar micropore structure for $\text{Cs}_4\text{PMo}_{11}\text{VO}_{40}$ to $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$.²⁴ However, at present, there is no direct evidence for the structure of the micropores in the crystallites of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$. Thus, further investigations are needed.

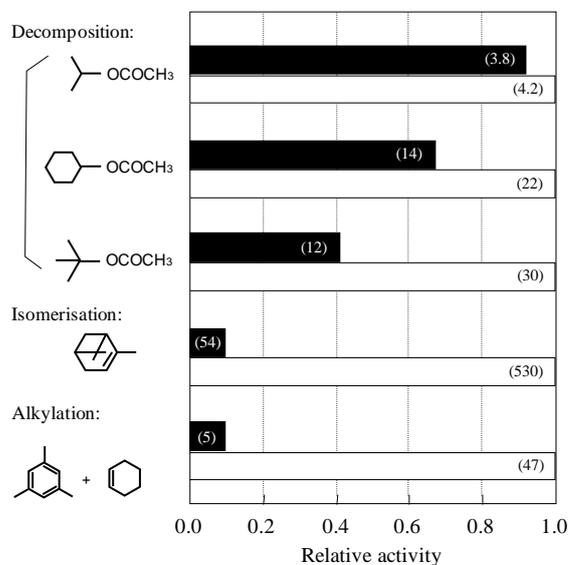


Figure 3. Relative activities of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ towards various kinds of reactions to those of $\text{Cs}_{2.5}\text{H}_{0.5}\text{PW}_{12}\text{O}_{40}$ (Cs2.5-*P*) in the liquid-solid reaction system. The catalytic activity of Cs2.5-*P* for each reaction is set to unity. The figures in the parentheses are the reaction rates in the unit of $\text{mmol g}^{-1} \text{ h}^{-1}$.

Figure 3 shows the relative catalytic activity of $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ for each reaction in relation to those of $\text{Cs}_{2.5}\text{H}_{0.5}\text{PW}_{12}\text{O}_{40}$ (abbreviated as Cs2.5-*P*). Cs2.5-*P* has been shown to have micropores with sizes of more than 0.75 nm^{17} and mesopores with sizes of ca. 4 nm^{16} and does not exhibit any size-selective catalytic activity due to its large pore size.¹⁵ As seen in Figure 3, Cs2.5-*P* catalyzed all of the reactions with considerable activities (the reaction rates are shown in the parentheses in Figure 3). On the other hand, although $\text{Cs}_3\text{HSiW}_{12}\text{O}_{40}$ was as active as Cs2.5-*P* towards the

decomposition of isopropyl acetate, the relative activity decreased in the following order: decomposition of isopropyl acetate > decomposition of cyclohexyl acetate > decomposition of *tert*-butyl acetate > isomerization of α -pinene \approx alkylation of 1,3,5-trimethylbenzene. Cs₃HSiW₁₂O₄₀ showed very low relative activity for the isomerization of α -pinene and alkylation of 1,3,5-trimethylbenzene. After the reactions of the decomposition of isopropyl acetate, Cs₃HSiW₁₂O₄₀ was recovered by a simple filtration from the mixture and dried at 373 K. The recovered Cs₃HSiW₁₂O₄₀ showed similar activity to the fresh one for the reactions. Critical sizes of the molecules were estimated from Van der Waals radii and a molecular model obtained by using MM2 calculations to be the following: isopropyl acetate (0.52 nm) < cyclohexyl acetate (0.53 nm) < *tert*-butyl acetate (0.54 nm) < α -pinene (0.61 nm) < 1,3,5-trimethylbenzene (0.77 nm). Although the critical size of *tert*-butyl acetate was similar to that of cyclohexyl acetate, the cross-sectional area of the former (0.54 nm \times 0.46 nm) was much larger than that of the latter (0.53 nm \times 0.37 nm). Therefore, the catalytic activity of Cs₃HSiW₁₂O₄₀ can be understood if the catalyst differentiates the reactant molecules according to their sizes; that is, it is size selective.

In the case of the Cs_x-P system, microporous Cs₂.1-P showed reactant size selectivity in the acid catalyzed reactions.¹⁵ Cs₂.1-P exhibited an activity for the dehydration of 2-hexanol but was inactive for the decomposition of isopropyl acetate due to the pore-size limitation.¹⁵ On the other hand, as seen in Figure 3, Cs₃HSiW₁₂O₄₀ showed reasonably high activity for the decomposition of isopropyl acetate. This indicates that the pore size of Cs₃HSiW₁₂O₄₀ is larger than that of Cs₂.1-P, which is consistent with the pore-size distributions shown in Figure 2. Therefore, Cs₃HSiW₁₂O₄₀ is a novel example of a heteropoly acid catalyst showing size selectivity in reactions with larger sized reactants.

Typical 12-membered oxygen ring zeolites, such as H- β , showed only one tenth of the activity of Cs₃HSiW₁₂O₄₀ for the decomposition of isopropyl acetate under the present reaction conditions. Since the pore size of H- β (0.76 nm \times 0.64 nm) is larger than the critical size of isopropyl acetate, the low activity was due to the weaker acid strength of the zeolites. Therefore, the strong acidity of Cs₃HSiW₁₂O₄₀ greatly contributes to the high activity towards the decomposition of isopropyl acetate and cyclohexyl acetate. We wish to emphasize that the much larger micropores and strong acidity of Cs₃HSiW₁₂O₄₀ expand the possible applications of microporous solid acids.

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