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<th>Title</th>
<th>Practical Preparation of Epilactose Produced with Cellobiose 2-Epimerase from Ruminococcus albus NE1</th>
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<td>Author(s)</td>
<td>Saburi, Wataru; Yamamoto, Takeshi; Taguchi, Hidenori; Hamada, Shigeki; Matsui, Hirokazu</td>
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1) Running title: Practical Preparation of Epilactose

2) Practical preparation of epilactose produced with cellobiose 2-epimerase from *Ruminococcus albus* NE1

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6) Abbreviations: CE, cellobiose 2-epimerase; RaCE, *R. albus* CE
Abstract

A practical purification method for a non-digestible disaccharide, epilactose (4-\(\beta\)-galactosyl-D-mannose) was established. Epilactose was synthesized from lactose by cellobiose 2-epimerase and purified by the following procedures: 1) removal of lactose by crystallization, 2) hydrolysis of lactose by \(\beta\)-galactosidase, 3) digestion of monosaccharides by yeast, and 4) column chromatography with Na-form cation exchange resin. Epilactose of 91.1% purity was recovered in 42.5% yield.

Key words: epilactose, cellobiose 2-epimerase, practical preparation
Epilactose (4-\(\beta\)-galactosyl-D-mannose) is a rare oligosaccharide, and is found in heated and alkali treated cow milk.\(^1,2\) This disaccharide is highly resistant to rat intestinal enzymes, and helps the strong proliferation of the human bifidobacteria \(Bifidobacterium bifidum, Bifidobacterium longum, Bifidobacterium breve,\) \(Bifidobacterium adolescentis,\) and \(Bifidobacterium catenulatum.\)\(^3\) Epilactose promotes Ca adsorption in the small intestine of rats more so than fructooligosaccharides, which are also known to enhance Ca adsorption.\(^4\) Recently, it was demonstrated that epilactose increased paracellular Ca adsorption in the small intestine through the induction of myosin light chain phosphorylation via myosin light chain kinase- and Rho-associated kinase-dependent mechanisms.\(^4\)

Cellobiose 2-epimerase (CE; EC 5.1.3.11) catalyzes the 2-epimerization of the glucose residue at the reducing end of cellobiose and produces 4-\(\beta\)-glucosyl-D-mannose. CEs were found in some anaerobic bacterium such as the ruminal strain \(Ruminococcus albus\) NE1,\(^5\) \(Eubacterium cellulosolvens,\)\(^6\) and \(Bacteroides fragilis\) NCTC9343.\(^7\) CE is also able to act on lactose to produce epilactose.\(^3\) However, studies on the properties of epilactose are limited by the low yields obtained by preparative TLC\(^3\) and HPLC\(^8\) used to purify the sugar after enzymatic synthesis. It takes a lot of effort to obtain even several gram of epilactose by these methods. Herein, we report a practical purification method of epilactose, which is suitable for scale up for industrial purposes.

The reaction of CE with lactose was performed using recombinant \(R.\) \(albus\) CE (RaCE) produced by \(Escherichia coli\) as described previously.\(^3\) One U of CE was defined as the enzyme amount that forms 1 \(\mu\)mol of epilactose from 20 mM lactose in 1 minute at 30°C in 100 mM sodium phosphate buffer (pH 7.5). RaCE (3,000 U) was added to 3 kg lactose monohydrate (Kanto Chemical Co., INC.; Tokyo, Japan) suspended in 15 L of 5 mM potassium phosphate buffer (pH 7.0). The reaction mixture was stirred and incubated at room temperature for 48 h. After the reaction, lactose was completely dissolved. The production of epilactose reached plateau, and 26.5% of
lactose was converted to epilactose. It indicated that 795 g of epilactose was produced.

The content of epilactose was measured by high performance liquid chromatography under following conditions: Sample concentration, 5% (w/v); injection volume, 10 µL; column, Sugar SP0810 (ϕ8.0 x 300 mm; Shodex, Tokyo, Japan); column temperature, 80°C; eluent, water; flow rate, 0.8 mL/minute; detection, refractive index. Authentic epilactose was purchased from Sigma (St. Louis, Missouri, USA) and used as standard.

The pH value of this solution was adjusted to pH 4.0 to avoid isomerization of epilactose and heated to 80°C to stop the enzymatic reaction. Then, the mixture was concentrated to about 60% (w/v) in vacuo and stored at 4°C for 1 day to crystallize the unreacted lactose. The crystallized lactose was removed by filtration and the filtrate was recovered. The lactose was washed by several hundred mL of ice-cold water. This filtrate was combined with the first filtrate (5 L in total), and using a differential refractometer (Atago, Co., Ltd.; Tokyo, Japan), the solution was found to contain 15.8% (w/w) of carbohydrate. The specific gravity was approximated by 1.0, and the measured value was identified as the carbohydrate concentration. It indicates that the recovered sample included 790 g of solid material. The crystallization of lactose is effective for the purification of epilactose, and increased the content of epilactose to 70.3%.

Produced epilactose of 555 g (69.8% of produced epilactose) was recovered and the purity of the epilactose was increased 2.6-fold.

The concentration of carbohydrate was adjusted to 10% (w/v) with water. Then, 1/100 vol of 1 M potassium phosphate buffer (pH 6.0) and 12,600 U of *Bacillus circulans* β-galactosidase (16 U per gram solid; Amano Enzyme Inc.; Nagoya, Japan) were added. One U of β-galactosidase was defined as the enzyme amount to liberate 1 µmol *o*-nitrophenol from 20 mM *o*-nitrophenyl β-galactoside in 1 minute at 40°C in 50 mM sodium acetate buffer (pH 6.0). The reaction mixture was incubated at 53°C for 3.5 h. Under these conditions, 57% and 16% of lactose and epilactose was hydrolyzed, respectively, when authentic sample was used as a substrate. The lactose in the sample was preferentially hydrolyzed to galactose and glucose and the content of lactose
decreased from 29.8% to 5.3%. On the other hand, epilactose was slightly hydrolyzed by this enzyme. After the reaction, mannose content was increased up to 4.0% of total carbohydrate. The reaction mixture was incubated at 80°C for 30 minutes to stop the reaction and then the mixture was cooled down to 30°C.

Baker’s yeast (15 g) (Kirin Kyowa Foods Ltd.; Tokyo, Japan) was added and stirred at 30°C overnight to digest monosaccharides. After yeast treatment, only monosaccharides, galactose and glucose, were successfully consumed and glycerol (3.8% of the solid material) was produced by the yeast. The mixture was centrifuged (7,000xg, 4°C, 5 minutes) and a supernatant was obtained. Then, several g of active carbon (Kirin Kyowa Foods Co. Ltd.; Tokyo, Japan) was added and incubated at 80°C for 30 minutes. The mixture was filtered with a diatomite filter and deionized by ion exchange column chromatography using Amberlite MB-4 (Rohm and Haas Co.; Philadelphia, PA, USA). The deionized mixture was filtered using a 0.45 µm membrane filter and concentrated in vacuo. A concentrate of 900 mL was obtained and the concentration of carbohydrate was 56.6% (w/v; specific gravity was 1.27). The solid material in the obtained sample was 647 g and the content of epilactose was 83.9%, indicating that 543 g of epilactose (68.3% of produced epilactose) was recovered.

Column chromatography using Na-form cation exchange resin, UBK530 (Mitsubishi Chemical Co.; Tokyo, Japan), which is often utilized in industrial processes, was performed. The conditions of chromatography were as follows: sample concentration, 50% (w/v); injection volume, 113 mL; column, UBK530 (φ28.0 x 550 mm x 4); column temperature, 80°C; flow rate, 11.3 mL/minute; fraction volume, 15 mL. Epilactose and glycerol were successfully separated using column chromatography, and the purity of epilactose was increased up to 93.3% (Fig. 1). The fractions containing more than 90% epilactose (fractions 45-57) were collected. The content of epilactose from the pooled fractions was 91.1% and the total carbohydrate was 32.4 g, indicating that 62.2% of epilactose applied to the column was collected. Based on this result, the total yield of purified epilactose from the reaction mixture of CE was estimated to be 42.5% (Table 1).
It was very difficult to achieve higher purity of epilactose with this system because of the lactose remaining after the β-galactosidase reaction. Therefore, it was thought that complete hydrolysis of lactose by β-galactosidase is required to achieve higher purity of epilactose. However, longer β-galactosidase treatment results in low yield due to degradation of epilactose. So β-galactosidase more specific to lactose was required. In this study, we established a practical purification method for epilactose, which can be scaled up for use in industrial processes. This method should prove useful for providing purified epilactose for further biological studies.

References
Table 1. Summary of the purification of epilactose.

<table>
<thead>
<tr>
<th>Procedure</th>
<th>Total sugar (g)</th>
<th>Epilactose (g)</th>
<th>Purity (%)</th>
<th>Yield (%)</th>
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<tbody>
<tr>
<td>Reaction mixture of CE*</td>
<td>3,000</td>
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<td>26.5</td>
<td>100</td>
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<tr>
<td>Crystallization of lactose</td>
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<td>555</td>
<td>70.3</td>
<td>69.8</td>
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<tr>
<td>Hydrolysis of lactose</td>
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<td>70.1</td>
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<td>Yeast treatment</td>
<td>647</td>
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<td>83.9</td>
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<td>UBK530 column chromatography</td>
<td>371**</td>
<td>338**</td>
<td>91.1</td>
<td>42.5</td>
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</table>

*, cellobiose 2-epimerase; **, estimated value based on the yield from the UBK530 column chromatography with a portion of the sample purified.
Fig. 1. Saburi et al.
Figure legends

Fig. 1. Elution pattern of UBK530 column chromatography.
Sample concentration, 50% (w/v); injection volume, 113 mL; column, UBK530 (ϕ28.0 x 550 mm x 4); column temperature, 80°C; flow rate, 11.3 mL/minute; fraction volume, 15 mL. The concentration of carbohydrate was measured with a differential refractometer. ●, total carbohydrate; ○, epilactose; ▲, lactose; △, glycerol; □, unknown.