Composition and Structure Changes in Al$_3$Ni$_2$ Microchannel Lining Layers by Alkali Leaching

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Abstract
Effects of alkali leaching time on the composition and structure changes in the Al$_3$Ni$_2$ microchannel lining layer produced by a sacrificial-core method have been investigated. The composition was measured both on the specimen surface directly exposed to the leachant and on the new surface cut after alkali leaching. In each surface, the decrease in Al concentration became sluggish after formation of Ni$_3$Al. On the other hand, nano structure consisted of almost pure Ni was detected on the inner wall of the microchannel leached for 864 ks.

Key words
Microchannel, Powder Metallurgy, Infiltration, Alkali Leaching, Nickel, Selective Leaching

1. Introduction
A metallic microreactor is suitable for catalyst reactions because it has high specific surface area and low flow resistance, which come from the microchannel structure. Additionally, it has good thermal shock resistance, high strength, and excellent heat conductivity. Some of the authors investigated the sacrificial-core method which was a simple powder-metallurgical process for producing the metallic microreactors [1-5]. In their experiments, they used two kinds of metals with different melting points: a body metal with higher melting point and a sacrificial-core metal. The body metal composes the device body, and the sacrificial-core metal gives the shape of the microchannel.

When nickel was used as the body metal and aluminum as the sacrificial-core metal, a porous thick film of Ni-Al intermetallic compounds formed as a lining layer. [4] Figure 1 depicts a Ni-Al binary alloy phase diagram. According to this diagram, the solid phase in equilibrium with Al-rich liquid changes depending on the temperature: Al$_3$Ni, Al$_3$Ni$_2$ and NiAl.

Catalytic activities of some Ni-Al intermetallic compounds were investigated [7-15]. Xu et al. reported that...

![Fig. 1 Ni-Al binary alloy phase diagram based on the report by Okamoto [6]](image1)

![Fig. 2 Schema of the powder metallurgical microchanneling process and alkali leaching treatment of the lining layer](image2)
alkali-leached Ni$_3$Al powder exhibit catalytic activity for hydrogen production from methanol or methane. [7-11] A mixture of Al$_3$Ni and Al$_3$Ni$_2$ is well known as a precursor alloy for Raney-Ni catalysts [12-15].

In our previous study [5], we found a heat treatment condition to produce a microchannel lining layer consisting of Al$_3$Ni$_2$, and attempted to control its composition by alkali leaching. Figure 2 illustrates the schema of our process combing the sacrificial-core method and the alkali leaching process. A green compact of nickel powder containing aluminum wire is sintered at a temperature between the melting points of these metals. During sintering of the green compact, molten aluminum migrates to the nickel powder region by infiltration and diffusion. These metals react and produce an intermetallic layer lining the microchannel formed at the sites initially occupied by the aluminum wire. Then, the lining layer is dipped in alkali solution for selective leaching of aluminum in order to give a catalytic activity to inner-wall surface of the microchannel. In our previous study, an Al$_3$Ni$_2$ microchannel lining layer was dipped in NaOH aqueous solution for 86.4 ks. As a result, the ratio of Al to Ni of the lining layer was decreased from 1.5 to 0.6, but porous Ni like Raney catalyst was not formed. Another shortcoming of our previous study was that the composition was measured only on the exposed surface of the specimens. Therefore, composition changes in the lining layer inside the microchannel were not clear.

In this study, we investigated the relationship between the alkali leaching time and the changes in the composition and structure of the Al$_3$Ni$_2$ microchannel lining layer inside the microchannel comparing with that on the specimen surface.

2. Experimental Procedure

2.1 Preparation of sintered compacts

We used 13.9 g of nickel powder and three aluminum wires as the body-metal powder and the sacrificial cores, respectively. The average diameter of the nickel powder was 5 µm. The sacrificial cores were 500 µm in diameter and 10 mm in length. The nickel powder containing the sacrificial cores was cold-pressed into a cylindrical green compact in a stainless steel mold using a unidirectional pressure of 460 MPa. The shape of the resultant compact specimen was a columnar 20 mm in diameter and 5 mm in height.

The green compacts were sintered in an argon gas atmosphere. Figure 3 illustrates the time-temperature pattern during the sintering heat treatment. The broken line in Fig. 3 indicates the standard pattern used for Ni-Al microchanneling experiments in the previous study [4].

2.2 Alkali leaching treatment

The specimen after sintering was cut to thickness of 5 mm and then polished. The microchannel penetrated the specimen in the thickness direction. The specimen after polished was dipped in a NaOH aqueous solution at 323 K in order to leach aluminum. The NaOH concentration of the aqueous solution was 7 kmol/m$^3$. The leaching time was varied from 0.6 to 2592 ks. The structures and compositions of the outer surface exposed to the leachant and a new surface cut after alkali leaching of the lining layer were measured by EPMA. Figure 4 shows the schema of the specimen with these surfaces. Additionally, the microstructure and composition of the inner-wall surface of the microchannel was observed by FE-SEM along with EDS.

3. Results and Discussions

Figure 5 shows back-scattered electron images of the exposed surfaces before and after alkali leaching and the new surface cut after alkali leaching. The leaching time was 86.4 ks. As seen in Figs. 5 (b) and (c), many cracks formed in the lining layer by alkali leaching. No other significant changes were observed in these photographs. The average composition of the lining layer was Al-40mol%Ni before alkali leaching. The compositions measured on the exposed surface and new surface of the lining layer were changed by alkali leaching to Ni-24mol%Al-33mol%O and Ni-25mol%Al-36mol%O, respectively. This result indicated that the lining layer was dealloyed and oxidized during or after alkali leaching. The crack formation in the leached lining layer was probably caused by tensile stress resulting from deflection of aluminum.

In the experiment, the new surface cut after alkali leaching did not contact with leachant. Therefore, the surface did not oxidize during alkali leaching. In general,
Raney-Ni catalysts are very easy to oxidize because of its huge specific surface area. For this reason, Raney-Ni catalysts are preserved in water or ethanol. The oxidation of the lining layer probably occurred during the structure observation after alkali leaching due to contact with the air. Tanaka et al. [16] reported that Al$_3$Ni$_2$ phase was directly transformed into Ni during alkali leaching. In Fig. 5, however, the lining layer after alkali leaching had a uniform brightness which corresponded to a uniform composition. In fact, EPMA results revealed that the composition of the alkali-leached lining layer were almost uniform.

Figure 6 shows the relationships between leaching time and the ratio of Ni concentration, $C_{Ni}$, to Al concentration, $C_{Al}$, on the exposed surface and new surface of the lining layer. The initial value of the ratio $C_{Al}/C_{Ni}$ was 1.5 for each surface. Gray bands in Fig. 6 correspond to the composition ranges of Al$_3$Ni$_2$, NiAl, Ni$_3$Al and Ni solid solution at 673K (see Fig. 1). The ratio $C_{Al}/C_{Ni}$ on the exposed surface of the lining layer decreased to the coexistence region of NiAl and Ni$_3$Al until $\tau = 7.2$ ks. After $\tau = 7.2$ ks, the decrease in $C_{Al}/C_{Ni}$ became sluggish. In the coexistence region of NiAl and Ni$_3$Al, the decreasing manner of $C_{Al}/C_{Ni}$ on the new surface is similar to that on the exposed surface. Before

![Image](image-url)

**Table 1** Relationship between $C_{O}/C_{Al}$ and the elapsed time after alkali leaching

<table>
<thead>
<tr>
<th>Leaching time (ks)</th>
<th>Time after leaching (ks)</th>
<th>$C_{O}/C_{Al}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.6</td>
<td>199.8</td>
<td>0.44</td>
</tr>
<tr>
<td>0.6</td>
<td>756.6</td>
<td>0.29</td>
</tr>
<tr>
<td>86.4</td>
<td>196.2</td>
<td>1.2</td>
</tr>
<tr>
<td>86.4</td>
<td>755.5</td>
<td>1.4</td>
</tr>
</tbody>
</table>
reaching the coexistence region of NiAl and Ni$_3$Al, $C_{\text{Al}}/C_{\text{Ni}}$ started to decrease after $\tau = 3.6$ ks and it decreased relatively slowly compared to the exposed surface. The leachant penetrated into the long and thin pores. Therefore, the reduction of $C_{\text{Al}}/C_{\text{Ni}}$ on the new surface started after a certain time elapsed. On both surfaces, the rate of decline of $C_{\text{Al}}/C_{\text{Ni}}$ reduced drastically after reaching the NiAl-Ni$_3$Al coexistence region. Ni$_3$Al is known to have a very high corrosion resistance. Aluminum leaching from the lining layer possibly became difficult due to the formation of the Ni$_3$Al phase.

The relationships between the leaching time and the ratio of O concentration, $C_{\text{O}}$, to $C_{\text{Al}}$ on the exposed surface and new surface of the lining layer are shown in Fig. 7. The initial value of the ratio $C_{\text{O}}/C_{\text{Al}}$ was almost 0 for each surface. The solid line in Fig. 7 indicates the index value $C_{\text{O}}/C_{\text{Al}} = 1.5$ which corresponds to the composition of Al$_2$O$_3$. It is noteworthy that the trend of increasing of $C_{\text{O}}/C_{\text{Al}}$ on each surface in Fig. 7 corresponded to that of decreasing of $C_{\text{Al}}/C_{\text{Ni}}$ in Fig. 6 respectively. $C_{\text{O}}/C_{\text{Al}}$ on the exposed surface reached 1.5 with shorter leaching time than that on the new surface. Aluminum is oxidized preferentially compared with nickel. Therefore, oxygen detected both on the exposed and new surfaces of the lining layer probably existed in the form of Al$_2$O$_3$ in the case when $\tau$ was shorter than 86.4 ks. When $\tau$ exceeded 864 ks, both Al and Ni oxidized owing to increase in the specific surface area.

Table 1 shows the relationship between $C_{\text{O}}/C_{\text{Al}}$ on the exposed surface of the lining layer and the elapsed time after alkali leaching in the air. According to this table, $C_{\text{O}}/C_{\text{Al}}$ was not changed from about 200 to about 760 ks for each leaching time. This result indicates that the oxidation of the alkali-leached lining layer was not a long time process such as atmospheric corrosion of iron.

The structures of the inner wall of the microchannels before and after alkali leaching are shown in Fig. 8. A needle-like structure was observed on the inner wall of the microchannel before alkali leaching (see Fig. 8 (a)). This structure is similar to the Al$_2$O$_3$ scale produced by high-temperature oxidation of NiAl [17]. Probably, the microchannel lining layer was oxidized by air slightly remained in the compact specimen. However, this structure had been completely dissolved after alkali leaching for 0.6 ks as shown in Fig. 8 (b). After leaching for 7.2 ks, fine asperities had formed on the inner wall of the microchannel as shown in Fig. 8 (c). This result indicates that the surface area of the microchannel can be increased by alkali leaching.

Figure 9 shows the relationship between the leaching time and the composition of the inner-wall surface of the lining layer.
microchannel. The Al, Ni and O concentrations were measured by EDS. It is noteworthy that almost pure Ni was detected on the specimen leached for 864 ks or longer. Figure 10 depicts the microstructure of the inner-wall surface of the microchannel after leaching for 864 ks. The structure has nano-scale spiny projections and it consists of almost pure Ni as we have intended in this study. This structure seems to have more orderly nature than that after 7.2 ks leaching (see Fig. 8 (c)). Possibly, reconstitution of the surface structure occurred after complete leaching, and as a result, the oxidizable nature of the surface was controlled. However, the detail mechanism is a subject for future study.

References
