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**A Rapid Synthesis of Hf-Beta Zeolite as Highly Active Catalyst for  
Meerwein-Ponndorf-Verley Reduction by Controlling Water Content  
of Precursor Gel**

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## 1 **Abstract**

2 Hf-Beta is a promisingly active Lewis acid catalyst for Meerwein-Ponndorf-Verley (MPV)  
3 reduction and other important organic reactions. However, the conventional hydrothermal synthesis  
4 of Hf-Beta inevitably requires the troublesome procedure for hydrolysis of tetraalkoxysilane and the  
5 long period to complete crystallization. In the present study, we applied a synthetic approach of  
6 reducing water content of precursor gel and succeeded in considerably shortening the period for  
7 crystallization of Hf-Beta using fumed silica as silicon source. By using precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2$   
8 = 1.4 – 7.6, effect of water content of precursor gel on the crystallization of Hf-Beta, the incorporation  
9 of Hf into the zeolite framework, and the catalytic performance were thoroughly investigated. Low  
10 water content was favorable for accelerating the crystallization, but unfavorable for the incorporation  
11 of Hf into the zeolite framework, resulting in poor catalytic activity. With the assistance of seed  
12 crystal, Hf-Beta with a relatively large amount of framework Hf was obtained from the precursor gel  
13 with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$  in 24 h. Hf-Beta synthesized in this way showed higher catalytic activity for  
14 MPV reduction than Hf-Beta as well as Zr-, and Sn-Beta synthesized by the conventional  
15 hydrothermal method.

16

## 17 **Keywords**

18 Hf-Beta; Lewis Acid; Metallosilicate; MPV Reduction; Zeolite

19

## 1 **1. Introduction**

2           MPV reduction is a useful reaction to produce alcohols from aldehydes or ketones under  
3 mild conditions. Traditionally, aluminum alkoxides [1-3] and metal complexes [3,4] are used as  
4 homogeneous Lewis acid catalysts for MPV reduction. Various types of heterogeneous catalysts have  
5 been studied for MPV reduction such as layered double hydroxides [5], metal oxides [6,7], supported  
6 metal alkoxides [3,8], and zeolites [9-20]. Of these materials, metallosilicate Beta zeolites with  
7 \*BEA-type structure containing tetravalent heteroatoms such as  $Ti^{4+}$ ,  $Zr^{4+}$ ,  $Sn^{4+}$ , and  $Hf^{4+}$  have  
8 emerged as highly active Lewis acid catalysts [10,12-20] with shape selectivity [10,12-16], tolerance  
9 against water [10,14], and recyclability [14]. In the last several years, Hf-Beta has been reported to  
10 show higher catalytic activity than metallosilicate analogues with Ti, Zr, and Sn for the MPV  
11 reduction of specific substrates [17-20].

12           Almost all of Hf-Beta samples reported so far were synthesized by the conventional  
13 hydrothermal method with hydrofluoric acid as mineralizing agent [17-20]. The conventional  
14 synthesis method successfully gives highly crystalline Hf-Beta with high catalytic activity, whereas  
15 it requires long period (several weeks) to complete the crystallization of Hf-Beta. In addition, when  
16 silicon alkoxide such as tetraethyl orthosilicate is used as silicon source, the alcohol produced by its  
17 hydrolysis must be removed from the precursor gel. To our knowledge, there has been only one  
18 alternative method, in which Hf-Beta was prepared by impregnating the Hf complex on dealuminated  
19 Beta [21]. In this method, extra-framework Hf species were generated, and post-synthetic acid  
20 treatment with concentrated nitric acid was required to remove them.

1           While there is limited variation of method for synthesis of Hf-Beta, several advanced  
2 methods have been developed for short-term synthesis of the other metasilicate Beta in simple  
3 manners [22-31]. For example, several groups reported the reduction of crystallization period for  
4 synthesis of Sn-Beta by decreasing the water content of precursor gel [23,24,26-28,30,31]. Yakimov  
5 et al. [26] reported that for synthesis of Sn-Beta with Si/Sn = 100, the crystallization period was  
6 reduced from 60 to 16 days by decreasing H<sub>2</sub>O/SiO<sub>2</sub> ratio in precursor gel from 6.8 to 5.6 and that  
7 the decrease in the water content did not affect the chemical state of Sn in the framework of Sn-Beta.  
8 Yang et al. [31] investigated in detail the crystallization profile and evolution of Lewis acid sites for  
9 Sn-Beta using precursor gel with H<sub>2</sub>O/SiO<sub>2</sub> = 4.5 and 7.5. The use of the precursor gel with lower  
10 water content resulted in faster crystallization and the number of Lewis acid sites for fully crystallized  
11 samples did not depend on the water content. Application of these methods to other zeolites is  
12 expected to bring shorter synthesis period and simplified procedure. However, the effect of water on  
13 the chemical state of heteroatoms in final products can vary from metal to metal, and the developed  
14 methods cannot always be applied to other metals by simply changing the metal source.

15           In the present study, Hf-Beta was synthesized from precursor gel with different H<sub>2</sub>O/SiO<sub>2</sub>  
16 ratios using fumed silica as silicon source. Effects of water content of precursor gel on the  
17 crystallization of zeolite and the incorporation of Hf into zeolite framework were thoroughly  
18 investigated. By using precursor gel with a low H<sub>2</sub>O/SiO<sub>2</sub> ratio, rapid crystallization was achieved,  
19 but the amount of Hf incorporated into the zeolite framework was only little. At the optimal H<sub>2</sub>O/SiO<sub>2</sub>  
20 ratio, Hf-Beta rich in framework Hf was successfully synthesized in a short period with the assistance

1 of seed crystal. In addition, Hf-Beta synthesized in this way showed higher catalytic activity for MPV  
2 reduction than Hf-Beta and other metallosilicate zeolites that were synthesized by the conventional  
3 hydrothermal method.

## 5 **2. Experimental**

### 6 **2.1. Materials**

7 Tetraethylammonium hydroxide (TEAOH, 35 wt.% aqueous solution), hafnium chloride  
8 ( $\text{HfCl}_4$ , 98 wt.%), and furfural ( $\geq 99.0\%$ ) were purchased from Sigma-Aldrich. Ammonium fluoride  
9 ( $\text{NH}_4\text{F}$ , 97%), hydrofluoric acid (47 wt.%), 2-propanol (98%), and *o*-xylene (98%) were purchased  
10 from FUJIFILM Wako Pure Chemical. 4-Methylcyclohexanone (98%), cinnamaldehyde ( $\geq 98.0\%$ ),  
11 and acetophenone ( $\geq 98.5\%$ ) were purchased from TCI. Fumed silica Aerosil<sup>®</sup> 300 was purchased  
12 from NIPPON AEROSIL. Deuterated acetonitrile ( $\text{CD}_3\text{CN}$ , 99.8% deuterated) was purchased from  
13 Cambridge Isotope Laboratories. Al-Beta (CP-814E with Si/Al = 12.5) was purchased from Zeolyst  
14 International.

### 16 **2.2. Synthesis of Hf-Beta**

17 Hf-Beta was synthesized by hydrothermal treatment of aqueous precursor gel, typically as  
18 follows. 0.107 g of  $\text{HfCl}_4$  was added to 7.56 g of TEAOH solution in 50 mL Teflon beaker, and the  
19 resulting mixture was stirred at 60 °C for 1 h. After cooling the mixture to ambient temperature, 2.0  
20 g of fumed silica was added with stirring. At this point, seed crystal corresponding to 1 wt. % of  $\text{SiO}_2$

1 was optionally added. The resulting suspension was further stirred at ambient temperature for 2 h.  
2 Then, 0.67 g of NH<sub>4</sub>F was added to the suspension. Considering the water contained in fumed silica  
3 (1.9 wt.%), the resulting gel had a molar composition of 1.0 SiO<sub>2</sub>: 0.55 TEAOH: 0.01 HfCl<sub>4</sub>: 0.55  
4 NH<sub>4</sub>F: 8.7 H<sub>2</sub>O. To obtain precursor gel with lower water content, the gel was heated at 60 °C to  
5 evaporate desired amount of water. The weight of the gel was measured before and after the heating,  
6 and the amount of water in the final precursor gel was estimated assuming that the weight loss during  
7 the heating was due to the evaporation of water. For several representative precursor gel samples, the  
8 actual water content was measured by the thermogravimetric analysis, and it was confirmed that the  
9 above estimation was correct. The volume of precursor gel with H<sub>2</sub>O/SiO<sub>2</sub> = 6.4 and 1.4 was 7.5 and  
10 4.6 mL, respectively. The precursor gel was transferred to a 100 mL Teflon-lined stainless-steel  
11 autoclave. The crystallization was done by heating the autoclave under static conditions at 180 °C for  
12 a set period. After the crystallization, the solid sample was recovered by filtration, washed with  
13 ethanol and Milli-Q water, and finally dried at 60 °C overnight. The as-synthesized sample was  
14 calcined in air at 650 °C for 6 h. Samples for different crystallization periods were obtained in separate  
15 synthesis batches following the aforementioned procedure.

16 The seed crystal was prepared by dealumination of the commercially available Al-Beta. 10  
17 g of Al-Beta was treated in 500 mL of 7.2 mol L<sup>-1</sup> HNO<sub>3</sub> solution at 80 °C for 24 h. The solid was  
18 recovered by suction filtration, washed with Milli-Q water, and dried at 60 °C overnight. Si/Al ratio  
19 of the dealuminated Beta (DeAl-Beta) was determined to be higher than 1000 by ICP-AES.

20 As a comparison, Hf-, Zr-, and Sn-Beta were prepared by the conventional hydrothermal

1 method with hydrofluoric acid [32], and are denoted as Hf-HF, Zr-HF, and Sn-HF, respectively.  
2 HfO<sub>2</sub>/Si-Beta was prepared by calcining the mixture of HfO<sub>2</sub> and Si-Beta, which was prepared by the  
3 conventional hydrothermal method.

### 5 **2.3. Characterization**

6 Powder XRD patterns of samples were collected on a Rigaku MiniFlex diffractometer with  
7 Cu K $\alpha$  radiation (30 kV, 15 mA,  $\lambda = 0.154$  nm) at a step width of 0.02°. Nitrogen sorption isotherms  
8 were measured on a MicrotracBEL BEL-mini analyzer at -196 °C. Prior to the measurement, samples  
9 were pretreated in nitrogen flow (50 mL min<sup>-1</sup>) at 400 °C for 1 h. Specific surface area was calculated  
10 by the Brunauer-Emmett-Teller (BET) method. Morphology of samples was observed by a FE-SEM  
11 using Hitachi S-4800 microscope at an acceleration voltage of 1 kV. Elemental analysis of solid  
12 samples was performed by ICP-AES using a Shimadzu ICPE-9000 analyzer. 10 mg of samples were  
13 added to 5 mL of 1 M KOH aqueous solution and heated at 100 °C for 30 min. The resulting solution  
14 was diluted with Milli-Q water and analyzed.

15 Acid properties of samples were examined by FT-IR spectroscopy with CD<sub>3</sub>CN as a probe  
16 molecule. FT-IR measurement was carried out on a JASCO FT/IR-4600 with a TGS detector with 64  
17 scans and 2 cm<sup>-1</sup> resolution in the range of 4000 – 400 cm<sup>-1</sup>. A powder sample (45 mg) was pelletized  
18 to a self-supporting disk with diameter of 2 cm and placed in a quartz IR cell with CaF<sub>2</sub> optical  
19 windows. The sample disk was pretreated at 400 °C for 1 h under vacuum. After the sample was  
20 cooled to 30 °C, the first spectrum of the bare sample was recorded. A dose of CD<sub>3</sub>CN with



1 predetermined pressure of 5 Pa was introduced into the cell. After the pressure became constant, a  
2 spectrum was recorded. Then, CD<sub>3</sub>CN was evacuated. This procedure was repeated with the dosing  
3 pressure of CD<sub>3</sub>CN increased up to 2000 Pa. Here, difference spectra between the first spectrum and  
4 the spectra after dosing CD<sub>3</sub>CN at certain pressure are shown. To compare the spectra quantitatively,  
5 spectra were normalized by using absorption bands of framework vibration at 1500 – 2100 cm<sup>-1</sup>.

6

## 7 **2.4. Catalytic reaction**

8 Catalytic performance of samples was evaluated in MPV reduction of various ketones and  
9 aldehydes such as 4-methylcyclohexanone (MCHOne), furfural, cinnamaldehyde, and acetophenone  
10 with 2-propanol (2-PrOH). Typically, MPV reduction of MCHOne with 2-PrOH was conducted as  
11 follows. A powder catalyst (25 mg) was added to 10 mL of 2-PrOH solution of MCHOne (0.5 mol L<sup>-1</sup>  
12 <sup>1</sup>) and *o*-xylene (internal standard, 0.015 mol L<sup>-1</sup>) in a test tube. The resulting suspension was heated  
13 at 70 °C with stirring for 1 h. The solid catalyst was separated by centrifugation and the supernatant  
14 solution was analyzed on a Shimadzu GC-2025 gas chromatograph equipped with a flame ionization  
15 detector and a capillary column (SH-Rtx-Wax, 30 m × 0.25 mm × 0.5 μm, Shimadzu). Substrate  
16 conversion and products yield were calculated from pre-drawn calibration curves using *o*-xylene as  
17 an internal standard.

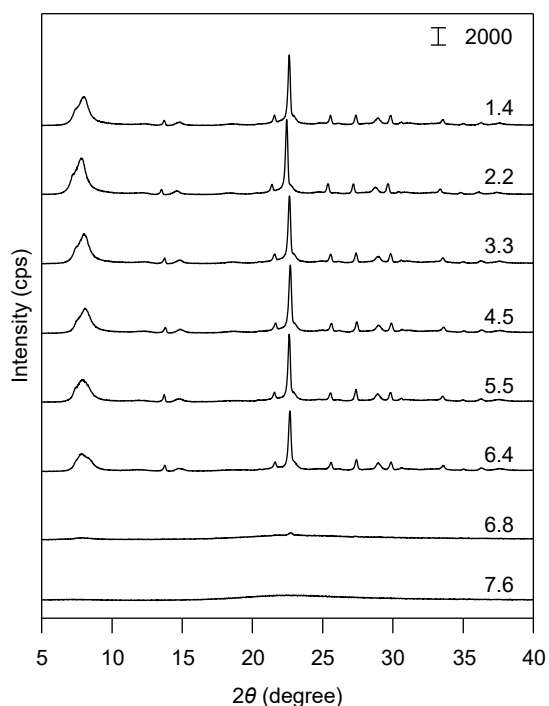
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## 19 **3. Results and Discussion**

### 20 **3.1. Influence of Water Content of Precursor Gel on Crystallization, Hf Incorporation**

## and Catalytic Activity

Influence of water content of precursor gel on crystallization of Hf-Beta was investigated by heating precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4 - 7.6$  at  $180\text{ }^\circ\text{C}$  for 72 h. Fig. 1 shows XRD patterns of samples calcined at  $650\text{ }^\circ\text{C}$ . The products obtained from the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4 - 6.4$  showed typical diffraction patterns assignable to \*BEA-type structure and no impurity phase was found. From the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.8$  and  $7.6$ , amorphous products were obtained, indicating that for the precursor gel with the high water content, crystallization did not proceed sufficiently under the present conditions. By using the precursor gel with low water content, Hf-Beta was successfully synthesized in far shorter period than that required for the conventional method typically using the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 \geq 7.5$  [17-20].



**Fig. 1.** XRD patterns of calcined samples synthesized from precursor gel with different water content. The numbers in the figure represent  $\text{H}_2\text{O}/\text{SiO}_2$  ratios of precursor gel.

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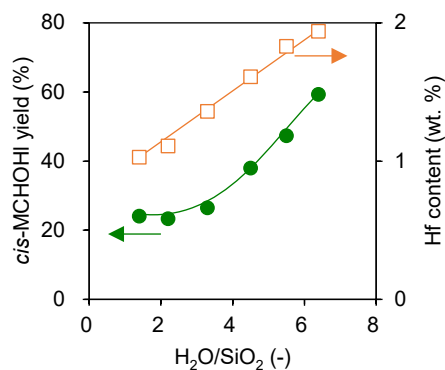
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11 **Fig. 2.** Influence of water content of precursor gel on Hf content (□) and catalytic activity (●) of Hf-

12 Beta. *cis*-MCHOH = *cis*-4-methylcyclohexanol.

13

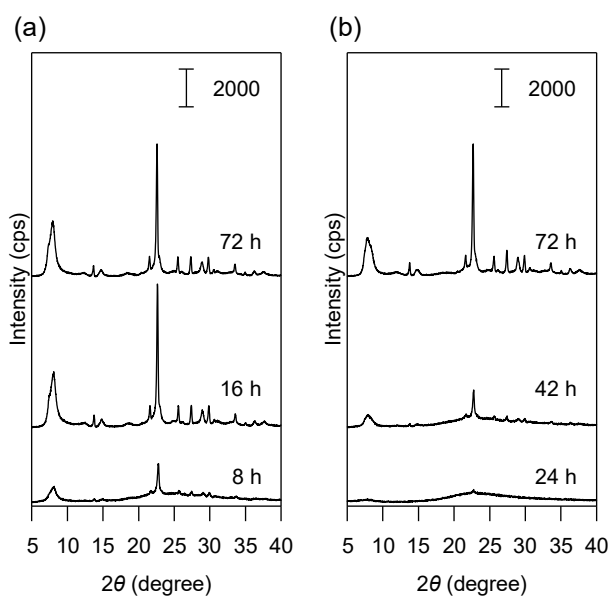
14 **3.2. Crystallization Process of Hf-Beta from Precursor Gel with H<sub>2</sub>O/SiO<sub>2</sub> = 1.4 and**

15 **6.4**

16 The precursor gel with H<sub>2</sub>O/SiO<sub>2</sub> = 1.4 and 6.4, selected as low and high water content

17 system, respectively, was heated at 180 °C for different periods to follow crystallization process of

1 Hf-Beta. In the synthesis using the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ , the diffraction lines of the  
2 (101) and (302) planes of the \*BEA-type structure were observed at  $7.9^\circ$  and  $22.7^\circ$ , respectively,  
3 even at 8 h (Fig. 3a). Upon extending the period to 16 h, the diffraction line intensity increased sharply.  
4 No further change was found in the diffraction pattern with further extension to 72 h. On the other  
5 hand, for samples from the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ , very weak diffraction lines first  
6 appeared at 24 h, and a highly crystalline sample was finally obtained in 72 h (Fig. 3b). For both  
7 systems, no crystalline impurity phase was found. Hereafter, the samples will be denoted as Hf- $x$ - $y$ ,  
8 where  $x$  and  $y$  represent  $\text{H}_2\text{O}/\text{SiO}_2$  ratio of precursor gel and crystallization period, respectively.



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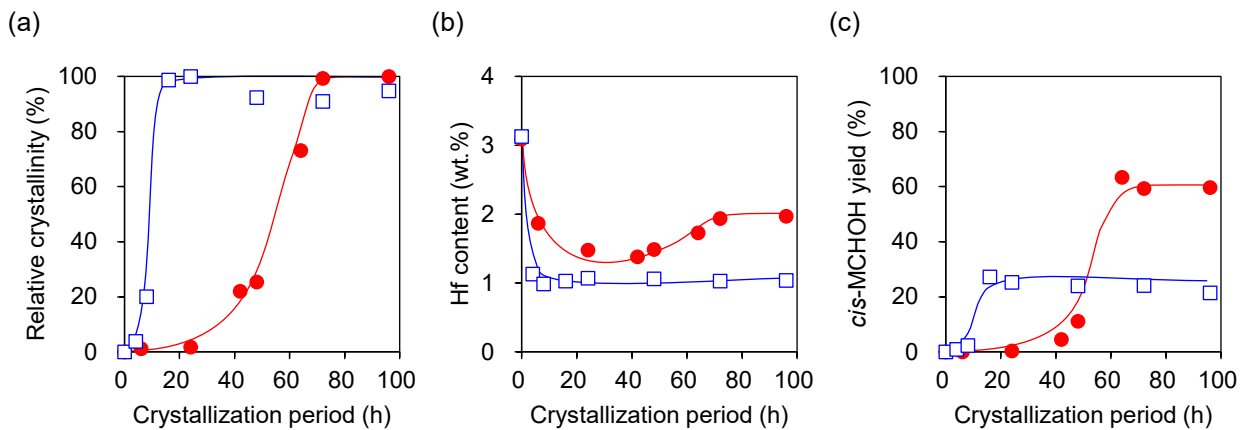
11 **Fig. 3.** XRD patterns of calcined samples synthesized from precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 =$  (a) 1.4  
12 and (b) 6.4 at different crystallization periods.

13

14 Relative crystallinity of samples from the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  and 6.4 were  
15 calculated based on the diffraction line intensities of Hf-1.4-16 and Hf-6.4-72, respectively (Fig. 4a).

1 For both systems, an induction period was observed before steep increase in the relative crystallinity.  
 2 A very short induction period of  $\sim 4$  h was observed for  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ , while a relatively long  
 3 induction period of  $\sim 30$  h was found for  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ . When the relative crystallinity increased,  
 4 there was also a difference in the slope of the curve between the two systems, and the crystallization  
 5 proceeded more rapidly for  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ . The relative crystallinity reached 90% at 16 and 72 h for  
 6  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  and 6.4, respectively. Weight yield of the solid products was  $\sim 90\%$  regardless of the  
 7 water content of precursor gel and the crystallization period.

8



9

10 **Fig. 4.** Temporal changes in (a) relative crystallinity, (b) Hf content, and (c) catalytic activity for MPV  
 11 reduction in course of crystallization of Hf-Beta from precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  ( $\square$ ) and 6.4  
 12 ( $\bullet$ ). *cis*-MCHOH = *cis*-4-methylcyclohexanol.

13

14 Fig. 4b shows variation of Hf content in the samples synthesized in both systems at different  
 15 crystallization periods. Both types of precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  and 6.4 were calcined without  
 16 hydrothermal treatment (crystallization time 0 h), and their Hf content was 3.1 and 3.0 wt.%,

1 respectively, which were almost the same as the amount of Hf added to the precursor gel. For  
2  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ , the Hf content decreased to 1.0 wt.% immediately after the start of hydrothermal  
3 treatment and did not change thereafter. For  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ , the Hf content was initially decreased  
4 to 1.4 wt.%. However, the Hf content turned to increase after 42 h, which synchronized with the  
5 relative crystallinity, shown in Fig. 4a. After 72 h, the Hf content reached a plateau at 1.9 wt.%.  
6 Therefore, it is concluded that in the synthesis using the precursor gels with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  and 6.4,  
7 the crystallization was completed in 16 and 72 h, respectively.

8           In order to track the missing Hf that was not found in the solid samples, elemental analysis  
9 was performed by ICP-AES for the solution remaining in the PTFE container after the hydrothermal  
10 treatment for synthesis of Hf-1.4-72, Hf-6.4-42, and Hf-6.4-72. However, Hf was not detected in  
11 these liquid samples, which implied that the missing Hf was mainly contained as unquantifiable Hf  
12 species in the solid samples. To confirm this,  $\text{HfO}_2/\text{DeAl-Beta}$  was prepared by calcining a mixture  
13 of  $\text{HfCl}_4$  and DeAl-Beta with  $\text{Si}/\text{Hf} = 100$  at 580 °C.  $\text{HfO}_2/\text{DeAl-Beta}$  showed very weak diffraction  
14 lines assignable to monoclinic  $\text{HfO}_2$ , and its  $\text{Si}/\text{Hf}$  ratio analyzed by ICP-AES was higher than 1000.  
15 These results demonstrated that extra-framework Hf species was poorly quantified by ICP-AES.  
16 Whereas, as explained above, the Hf species dispersed in the precursor gel without hydrothermal  
17 treatment was quantitatively analyzed. Hence, it is considered that the missing Hf was mainly  
18 contained in the solid samples as unquantifiable Hf species such as extra-framework Hf species and  
19 that the Hf content determined by ICP-AES indicated the amount of Hf well dispersed in the zeolite  
20 framework.

1 Yakimov et al. [26] reported that in the synthesis of Sn-Beta, the Sn content did not depend  
2 on the water content of precursor gel and almost all of Sn in the precursor gel was incorporated into  
3 the zeolites. In contrast, it is clearly shown that in the present synthesis of Hf-Beta, the Hf content  
4 strongly depended on the water content of the precursor gel and that the high water content was  
5 favorable for incorporation of Hf into the zeolite framework. The pH of the solution remaining after  
6 the hydrothermal treatment for Hf-1.4-72, Hf-6.4-42, and Hf-6.4-72 ranged from 9 to 10. The  
7 solubility of Hf in such weakly basic aqueous solution is one to two orders of magnitude lower than  
8 that of Sn [33,34]. Considering these points, the different feature of Hf and Sn for the incorporation  
9 into the zeolite framework was attributed to the difference in solubility of Hf and Sn in basic aqueous  
10 solution. It is presumed that a part of Hf might precipitate during the hydrothermal treatment, resulting  
11 in less incorporation into the zeolite framework. Accordingly, as the water content of precursor gel  
12 increased, the amount of such precipitated Hf decreased and Hf-Beta with high Hf content crystallized.

13 For both types of precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$  or  $6.4$ , insufficiently crystallized  
14 samples showed poor catalytic activity for the MPV reduction of MCHOne (Fig. 4c). Hf-1.4-16,  
15 which was a highly crystallized sample, gave 27% yield of *cis*-MCHOH. Further extension of the  
16 crystallization period did not change the catalytic activity of the samples synthesized from the  
17 precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ . For the samples from the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ ,  
18 catalytic activity appeared with crystallization period of 42 h or longer. The activity increased as the  
19 Hf content increased, and Hf-6.4-72 gave 59% yield of *cis*-MCHOH.

20 Focusing on geometric isomers of MCHOH, thermodynamically favorable *trans* isomer was

1 preferentially produced by using aluminum isopropoxide, which is a typical homogeneous catalyst  
 2 (Table 1, Entry 1). All of Hf-Beta gave thermodynamically unfavorable *cis* isomer as a predominant  
 3 product (Entries 2-4). It is known that since the formation of the *cis* isomer takes more compact  
 4 transition state than that for the *trans* one, the *cis* isomer is shape-selectively produced in the  
 5 micropores of the \*BEA-type structure [35]. These results clearly showed that the MPV reduction  
 6 proceeded shape-selectively in the micropores of Hf-Beta samples, demonstrating that framework Hf  
 7 atoms were the active sites over Hf-Beta.

8

9 **Table 1** Hf content, specific surface area, and catalytic activity of Hf-Beta samples.

Entry	Sample	Hf content <sup>a</sup> (wt.%)	$S_{\text{BET}}$ <sup>b</sup> (m <sup>2</sup> g <sup>-1</sup> )	MCHOH yield (%)		TON <sup>c</sup> (-)
				<i>cis</i>	<i>trans</i>	
1	Al( <sup>i</sup> Pr) <sub>3</sub>	-	-	22	41	-
2	Hf-1.4-72	1.0	626	24	1	888
3	Hf-4.5-72	1.6	611	38	1	864
4	Hf-6.4-72	1.9	566	59	2	1091

10 <sup>a</sup>Hf content determined by ICP-AES. <sup>b</sup>Specific surface area calculated by the BET method. <sup>c</sup>Turnover number  
 11 calculated as total amount of MCHOH (mol) per amount of Hf (mol) in a catalyst.

12

13 Acid properties of representative Hf-Beta samples were investigated by IR spectroscopy  
 14 with CD<sub>3</sub>CN as a probe molecule. From the experiments with dosing pressure of CD<sub>3</sub>CN varied, the  
 15 adsorption on Lewis acid sites was found to be saturated at dosing pressure of 200 Pa (Fig. S4). Fig.  
 16 5a compares absorption bands of C≡N stretching vibration of CD<sub>3</sub>CN adsorbed on Hf-1.4-72, Hf-4.5-  
 17 72, and Hf-6.4-72 at the dosing pressure of 200 Pa. As in an example of Hf-6.4-72 shown in Fig. S5,  
 18 these spectra were deconvoluted into four components with the peaks at 2313, 2307, 2299, and 2275

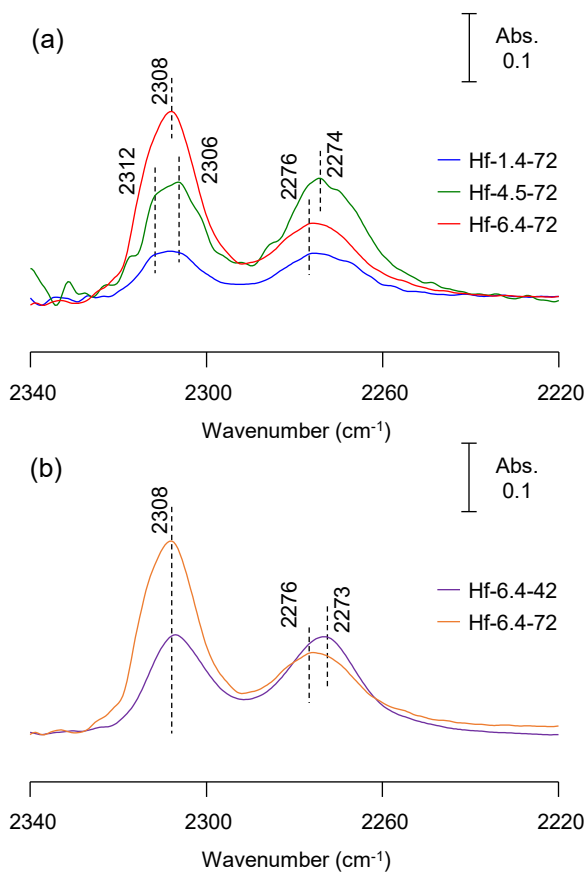


1  $\text{cm}^{-1}$ . Two similar peaks above  $2300 \text{ cm}^{-1}$  have been also found in adsorption of  $\text{CD}_3\text{CN}$  on Sn-Beta  
2 and attributed to the adsorption on Sn atoms in different coordination environments [36,37]. With  
3 reference to the reports on Sn-Beta, the two peaks above  $2300 \text{ cm}^{-1}$  are assigned to the adsorption on  
4 framework Hf with Lewis acid character [19,38]. The peak at  $2299 \text{ cm}^{-1}$  was attributed to adsorption  
5 on extra-framework Hf, as  $\text{HfO}_2/\text{Si-Beta}$  mainly showed an absorption peak at  $2299 \text{ cm}^{-1}$  (Fig. S6).  
6 The peak observed at  $2275 \text{ cm}^{-1}$  is assigned to adsorption on silanol groups [39,40].

7         The total area of the peaks at  $2313$  and  $2307 \text{ cm}^{-1}$  for Hf-1.4-72, Hf-4.5-72, and Hf-6.4-72  
8 was  $0.9$ ,  $1.6$ , and  $4.0 \text{ cm}^{-1}$ , respectively. This increasing trend indicated that as the water content of  
9 precursor gel increased, a larger number of Lewis acid sites were formed. Turnover numbers per Hf  
10 atom (TONs) of Hf-1.4-72 and Hf-6.4-72 were  $888$  and  $1091$ , respectively (Table 1, Entries 2 and 4).  
11 The larger TON for Hf-6.4-72 suggested that as the water content of precursor gel increased, the  
12 proportion of Hf that acted as Lewis acid sites increased as well. This indicates that Hf was likely to  
13 be incorporated into the zeolite framework and efficiently form Lewis acid sites under  $\text{H}_2\text{O}$ -rich  
14 conditions.

15         To trace the evolution of framework Hf during the hydrothermal treatment, Hf-6.4-42 was  
16 also investigated by IR with  $\text{CD}_3\text{CN}$  and compared with Hf-6.4-72 (Fig. 5b). The peaks attributed to  
17 adsorption on Lewis acid sites were also observed and the total peak area of those peaks was  $1.3$  and  
18  $4.0 \text{ cm}^{-1}$  for Hf-6.4-42 and Hf-6.4-72, respectively. Thus, the number of Lewis acid sites was greatly  
19 increased after 42 h. This increase coincided with those in the relative crystallinity and the Hf content  
20 (Fig. 4a and 4b).

1



2

3 **Fig. 5.** FT-IR spectra of CD<sub>3</sub>CN adsorbed on Hf-Beta (a) synthesized from precursor gel with different  
4 water content and (b) synthesized in different crystallization periods. Dosing pressure of CD<sub>3</sub>CN was  
5 200 Pa.

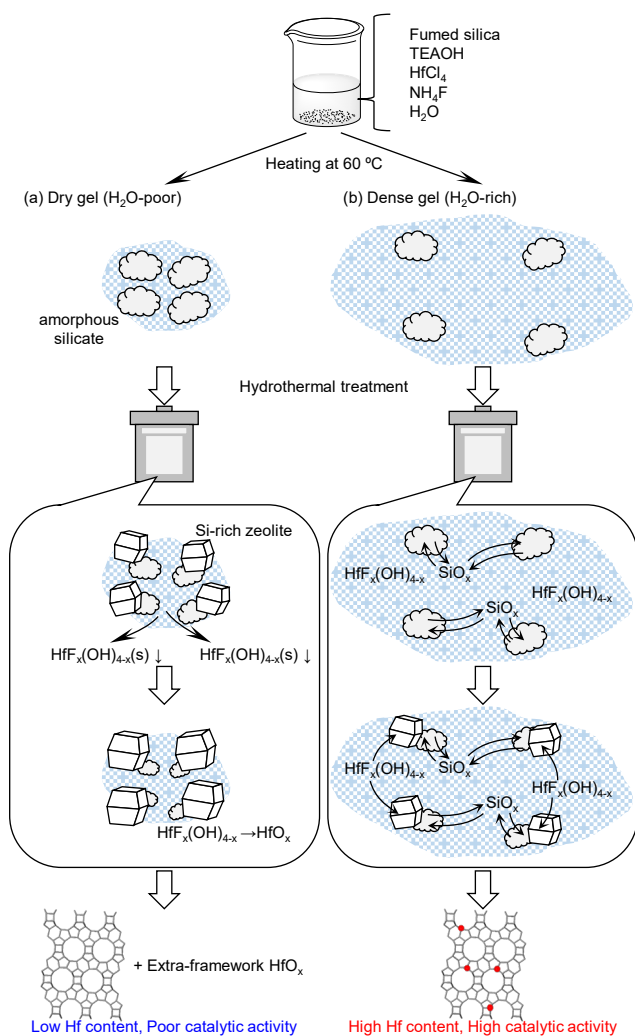
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7 Based on the results so far, we propose the role of water in precursor gel in the hydrothermal  
8 synthesis of Hf-Beta as Fig. 6. Generally, aqueous precursor gel separated into solid and aqueous  
9 solution during hydrothermal treatment, and metallosilicate species dissolved in the solution  
10 deposited onto the solid (nuclei) together with silicate to proceed crystallization. In the present  
11 synthesis, regardless of the water content of precursor gel, the Hf content decreased sharply at the  
12 very beginning of the hydrothermal treatment and the induction period was present before increase

1 in the relative crystallinity (Fig. 4). It is considered that because of the low solubility of Hf species in  
2 weakly basic solution, a part of Hf species in the solution precipitated, which gave extra-framework  
3 Hf species eventually. Since such extra-framework Hf species was unquantifiable by ICP-AES, the  
4 Hf content was decreased immediately after the start of hydrothermal treatment. The induction period  
5 was attributed to the period taken for nucleation enough for the following growth of nuclei.

6         When the water content of precursor gel was low ( $H_2O/SiO_2 = 1.4$ ), the precipitation was  
7 significant and only a limited amount of Hf in the solution was incorporated into the zeolite  
8 framework, resulting in the formation of zeolites with the low Hf content (Fig. 6a). When the water  
9 content of precursor gel was high ( $H_2O/SiO_2 = 6.4$ ), Si-rich nuclei formed during the induction period  
10 and then Hf species in the solution deposited onto the nuclei in the form of hafnosilicate and Hf was  
11 effectively incorporated into the zeolite framework (Fig. 6b). As the water content of precursor gel  
12 increased, the amount of precipitated Hf species decreased and Hf-Beta with the high Hf content  
13 crystallized. Similar crystallization mechanism in which Si-rich nuclei formed first and grew with the  
14 incorporation of heteroatoms was proposed for other metallosilicate zeolites [41-43].

15



**Fig. 6.** Plausible mechanism for crystallization of Hf-Beta from (a) H<sub>2</sub>O-poor or (b) H<sub>2</sub>O-rich precursor gel.

### 3.3. Accelerated crystallization of Hf-Beta with assistance of seed crystal

DeAl-Beta as seed crystal (1 wt.% of SiO<sub>2</sub>) was added to the precursor gel with H<sub>2</sub>O/SiO<sub>2</sub> = 1.4 and 6.4 to accelerate the crystallization of Hf-Beta. Samples synthesized with the seed crystal are designated with “-seed” at the end of their names. From the precursor gel with H<sub>2</sub>O/SiO<sub>2</sub> = 1.4 and 6.4, diffraction patterns of \*BEA-type structure appeared in 3 and 12 h, respectively, and the induction period was significantly shortened (Figs. 7a and S7). The seed crystal promoted the

1 generation of nuclei during the hydrothermal treatment, so that the induction period for the nucleation  
2 was shortened. For the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ , the relative crystallinity increased sharply  
3 at 12 h, demonstrating that the growth of nuclei was accelerated by the addition of seed crystal. Even  
4 for the synthesis with seed crystal, the solid yield was  $\sim 90\%$ , which was almost the same as that  
5 without seed.

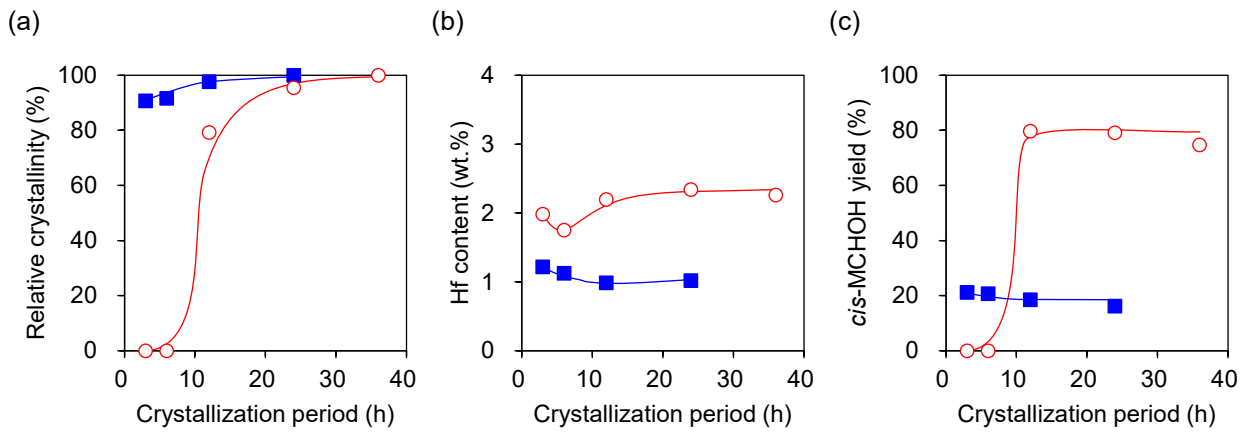
6           When the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$  was used, the Hf content decreased to 1.8 wt.%  
7 in 6 h but increased after 12 h and was 2.3 wt.% after 24 h (Fig. 7b). The behavior in which the Hf  
8 content decreased once and then increased with the progress of crystallization was also observed in  
9 the synthesis without the addition of the seed crystal (Fig. 4b). The Hf content was slightly higher  
10 when seed crystal was added. It is speculated that the seed crystal provided silicate species different  
11 from that provided by fumed silica into the solution, which was prone to condense with Hf into  
12 hafnosilicate, so that the amount of Hf finally incorporated into the zeolite framework increased.

13           For samples from the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ , catalytic activity appeared in  
14 crystallized ones after the synthesis period of 12 h (Fig. 7c), and the yield of *cis*-MCHOH reached a  
15 maximum of 79%. This activity was higher than that of Hf-HF, which was synthesized by the  
16 conventional hydrothermal method. On the other hand, for the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$ , the  
17 Hf content and catalytic activity was not increased by the addition of seed crystal.

18           Hf-6.4-24-seed showed the absorption peaks attributed to adsorption on Lewis acid sites and  
19 silanol groups in an IR spectrum with  $\text{CD}_3\text{CN}$  (Fig. S8). The total peak area assigned to adsorption  
20 on Lewis acid sites was  $5.4 \text{ cm}^{-1}$ . In this way, highly active Hf-Beta was successfully synthesized in

1 the very short period with the addition of seed crystal to the precursor gel with  $\text{H}_2\text{O}/\text{SiO}_2 = 6.4$ .

2



3

4 **Fig. 7.** Temporal changes in (a) relative crystallinity, (b) Hf content, and (c) catalytic activity for MPV

5 reduction in course of crystallization of precursor gel containing seed crystal with  $\text{H}_2\text{O}/\text{SiO}_2 = 1.4$

6 (■) and 6.4 (○). Relative crystallinity was calculated from intensity of the diffraction line at  $22.7^\circ$ ,

7 based on those of Hf-1.4-24-seed and Hf-6.4-36-seed, respectively. *cis*-MCHOH = *cis*-4-

8 methylcyclohexanol.

9

10 Particle morphology of representative samples was observed by SEM. Rounded octahedral

11 particles were observed for Hf-1.4-72 (Fig. 8a), and truncated octahedral particles typical for Beta

12 zeolite were observed for Hf-6.4-72 (Fig. 8b). The size of both samples was  $\sim 10 \mu\text{m}$ . Hf-1.4-12-seed

13 had spherical particles with uneven surface (Fig. 8c). For Hf-6.4-24-seed, truncated octahedral

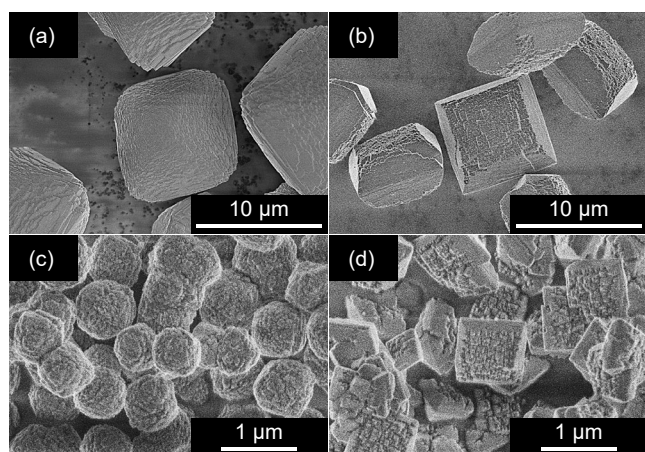
14 particles were majorly formed and random-shaped particles were minorly present (Fig. 8d). The

15 particle size of these two samples was reduced to  $\sim 1 \mu\text{m}$  by the addition of seed crystal. Because the

16 seed crystal promoted the generation of nuclei, the particle size of the grown crystal was reduced. Hf-

1 6.4-72 showed much higher activity than Hf-1.4-12-seed despite its larger particle size (Fig. 4c and  
2 7c). In addition, Hf-1.4-72 and Hf-1.4-12-seed showed similar activity despite the large differences  
3 in particle size. These results implied that the catalytic activity was determined by the Hf content and  
4 the nature of Hf, independent of the particle size.

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7 **Fig. 8.** SEM images of Hf-Beta. (a) Hf-1.4-72, (b) Hf-6.4-72, (c) Hf-1.4-12-seed, and (d) Hf-6.4-24-  
8 seed.

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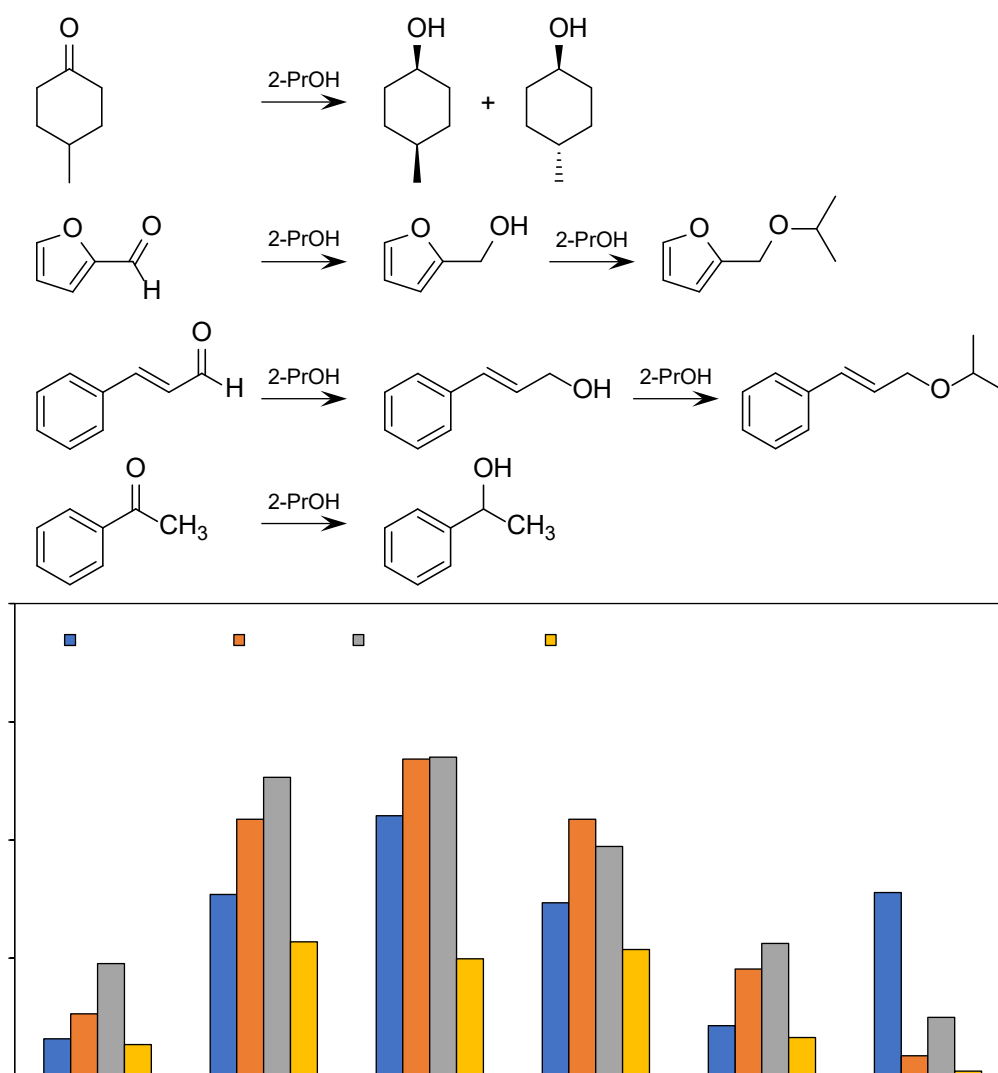
### 10 **3.4. Catalytic performance of Hf-Beta for MPV reduction of various carbonyl** 11 **compounds**

12 Catalytic performance of Hf-1.4-72, Hf-6.4-72, Hf-6.4-24-seed and metallosilicate zeolites  
13 synthesized by the conventional hydrothermal method (Hf-, Zr- and Sn-HF) were compared in MPV  
14 reduction of several carbonyl compounds. (Fig. 9). In addition to MCHOne, furfural, cinnamaldehyde,  
15 and acetophenone were also used as substrates of MPV reduction. In the reaction of furfural, the  
16 corresponding acetal was also produced in addition to furfuryl alcohol. The yield of acetal was ~8%  
17 for any catalyst, which was almost the same as that in the reaction without a catalyst. The acetalization

1 proceeded in parallel with the MPV reduction regardless of catalysts, and so the acetal yield was  
2 excluded from the evaluation of catalytic activity. The corresponding ether was also produced in the  
3 reduction of cinnamaldehyde, and the total yield of cinnamyl alcohol and the ether was used as the  
4 product yield of MPV reduction. In the reaction of MCHOne and acetophenone, the corresponding  
5 alcohols were the sole products. Please note that reaction results of MCHOne shown in Fig. 9 are the  
6 results obtained by reducing the amount of catalyst from the standard conditions in order to suppress  
7 the conversion/product yields.

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2 **Fig. 9.** Catalytic activity of Hf-Beta and other metallosilicate zeolite Beta for MPV reduction. *cis*-

3 MCHOH = *cis*-4-methylcyclohexanol, FurOH = Furfuryl alcohol, CinOH = Cinnamyl alcohol,

4 PhEtOH = 1-phenylethanol. Reaction conditions for MCHOne: Catalyst, 15 mg; MCHOne, 5 mmol;

5 2-PrOH, 10 mL; Temperature, 70 °C; Time, 1 h. Reaction conditions for furfural: Catalyst, 25 mg;

6 Furfural, 5 mmol; 2-PrOH, 10 mL; Temperature, 70 °C; Time, 1 h. Reaction conditions for

7 cinnamaldehyde: Catalyst, 100 mg; cinnamaldehyde, 5 mmol; 2-PrOH, 10 mL; Temperature, 70 °C;

8 Time, 1 h. Reaction conditions for acetophenone: Catalyst, 50 mg; Acetophenone, 5 mmol; 2-PrOH,

9 10 mL; Temperature, 70 °C; Time, 24 h.

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Hf-6.4-72 and Hf-6.4-24-seed gave much higher alcohol yields than Hf-1.4-72 for any substrate. The higher activity of Hf-6.4-24-seed and Hf-6.4-72 was due to the larger number of Lewis acid sites (Figs. 5 and S5). These two samples showed high activity for the MPV reduction of cinnamaldehyde, which is a conjugated enone, as well. Acetophenone required a long reaction time due to its significantly lower reactivity than other substrates, but Hf-6.4-24-seed and Hf-6.4-72 still showed high activity for the reduction of acetophenone.

Catalytic activity of Hf-HF, Zr-HF, and Sn-HF for MPV reduction of the three substrates except for MCHOne was decreased in the order of Hf-HF > Zr-HF > Sn-HF. On the whole, Hf-Beta showed excellent catalytic performance for MPV reduction. Turnover numbers per metal atom (TONs) for reduction of furfural of these zeolites were 840, 355, and 62, respectively (Table 2). Considering that the active sites on these Beta zeolites for MPV reduction are the framework metal atoms in common [12-18,20], the high TON of Hf-HF reflected the inherent high activity of Hf for MPV reduction. It was reported that the catalytic activity of Ti-, Zr-, and Sn-Beta for MPV reduction varied following the complex manner of electron donation/back donation between the metals and the substrates, strongly depending on the types of substrates [15]. Such a complex electronic effect could account for the exceptional high activity of Sn-Beta for the MPV reduction of MCHOne. Hf-6.4-24-seed and Hf-6.4-72 showed similar or slightly higher activity than Hf-HF synthesized by the conventional method, which demonstrated that the present method is excellent for efficiently synthesizing highly active Hf-Beta with high Hf content in a short period.

1  
2 **Table 2** Metal content and catalytic activity of metallosilicate zeolite samples.

Sample	Metal content <sup>a</sup> (wt.%)	FurOH yield <sup>b</sup> (%)	TON <sup>c</sup> (-)
Hf-1.4-72	1.0	11	381
Hf-6.4-72	1.9	44	771
Hf-6.4-24-seed	2.3	54	807
Hf-HF	1.8	44	840
Zr-HF	0.9	18	355
Sn-HF	1.3	4	62

3 <sup>a</sup>Metal content determined by ICP-AES. <sup>b</sup>Yield of furfuryl alcohol. <sup>c</sup>Turnover number calculated as amount of  
4 FurOH (mol) per amount of metal (mol) in a catalyst.

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## 7 **4. Conclusions**

8 Hf-Beta samples were synthesized from precursor gel with different water content. The  
9 lower water content allowed the fast crystallization of \***BEA**-type framework. However, because of  
10 the low solubility of Hf in weakly basic solution, precipitation of Hf species was significant during  
11 the hydrothermal treatment with low water content, resulting in the less incorporation of Hf into the  
12 zeolite framework and the poor catalytic activity for MPV reduction. Thus, in order to synthesize  
13 active Hf-Beta with high Hf content, it is necessary to use precursor gel with relatively high water  
14 content, but not too high. The role of water was considered to suppress precipitation of Hf species  
15 and hold it in the form of hafnosilicate during the nucleation period. By using precursor gel with the  
16 appropriate water content ( $H_2O/SiO_2 = 6.4$ ), highly active Hf-Beta zeolite was obtained in far shorter  
17 period than that required for the conventional hydrothermal method. With the assistance of seed  
18 crystal, the synthesis period was shortened to 24 h. Hf-6.4-24-seed and Hf-6.4-72 with the high Hf

1 content showed outstandingly high activity for the MPV reduction of several substrates and higher  
2 activity than metallosilicate zeolites that were synthesized by the conventional hydrothermal method,  
3 demonstrating that the present method is excellent for efficiently synthesizing highly active Hf-Beta  
4 with high Hf content in a short period.

5

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## 7 **Supporting Information**

8 Detailed data on characterization of samples are available in Supporting Information.

9

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12 ICP-AES was conducted with the instrument at the Institute for Catalysis, Hokkaido University. This  
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14

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