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Diagrams of Temperature-Distribution in a Thick Plate.

By Isao Suzuki.

(1946, 3, 1.)

Synopsis.

The temperature distributions in a thick plate, when one surface is heated, are numerically calculated and represented by diagrams as the functions of time and distance from the surface.

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1. Introduction.

Practically it may be necessary for engineers to know the influences, which the abrupt change of the temperature of the surface yields. When a plane surface of a semi-infinite domain is heated and kept at a constant temperature for some duration m , the temperature in the domain will increase at first and decrease gradually. The temperature distribution must be a function of time t and the distance x from the surface. As the first example, the calculations are carried out about this case; the time duration m of heating being taken as a parameter. As the second example, the heat distributions in the thick plate are calculated; the one of the surfaces is heated and the other is thermally insulated. Practically the temperature distribution in most cases can be looked upon as the intermediated case of these two extreme examples.

2. Heat Conduction of the Semi-infinite Solid.

In this paragraph the temperature distributions are calculated when the solid is bounded by the plane $x = 0$ and extends to infinity in the direction of x positive, and the isothermal surfaces are planes parallel to $x = 0$ and the flow of heat is linear, the lines of flow being parallel to the axis of x .

Let the initial temperature be given by $u = 0$, and the surface temperature vary with the time and the temperature at infinite boundary be zero. Then, in the semi-infinite solid, where u has to satisfy

$$\frac{\partial u}{\partial t} = a^2 \frac{\partial^2 u}{\partial x^2}, \quad \dots \dots \dots (1)$$

$$\begin{aligned} u &= 0 & \text{when} & \quad t = 0, \\ u &= f(t) & \text{at} & \quad x = 0, \\ \text{and } u &= 0 & \text{at} & \quad x = \infty, \end{aligned}$$

the solution is given by

$$u = \frac{x}{2a\sqrt{\pi}} \int_0^t \frac{f(\tau) e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau. \quad \dots \dots \dots (2)$$

The constant a^2 is called the diffusivity of that substance, or its thermometric conductivity,* and it is denoted by

$$a^2 = \frac{\kappa}{c\rho},$$

where κ = thermal conductivity of the substance,

c = specific heat of it,

and ρ = density of it.

Now let the temperature $u=f(t)$ at $x=0$ be in such a state that temperature keeps constant for a certain duration and then it falls, as shown in Fig-1.,

$$\begin{aligned} f(t) &= k & \text{when} & \quad 0 \leq t \leq m \\ \text{and } f(t) &= \frac{k}{n-m}(n-t) & \text{when} & \quad m \leq t \leq n. \end{aligned}$$

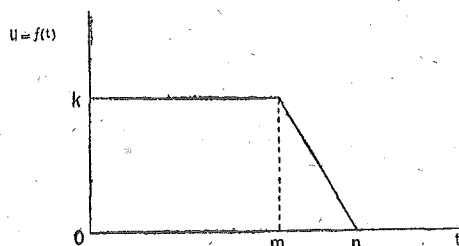


Fig. 1

In this case, in order to obtain the relations between time t and temperature u at a certain depth x , we must investigate the following four cases :

(1) when the surface temperature $f(t) = k$ continues infinitely, temperature at t is given by

$$u_1 = \frac{kx}{2a\sqrt{\pi}} \int_0^t \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau. \quad \dots \dots \dots (3)$$

(2) when the surface temperature $f(t) = k$ breaks off at time m , temperature at $t(>m)$ is given by

$$u_2 = \frac{kx}{2a\sqrt{\pi}} \int_0^m \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau. \quad (t > m) \quad \dots \dots \dots (4)$$

(3) when the surface temperature decreases with time from $t=m$ and becomes zero at $t=n$, temperature at t (between m and n) is given by

$$\begin{aligned} u_3 &= \frac{kx}{2a\sqrt{\pi}} \int_0^m \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau + \frac{kx}{2a\sqrt{\pi}} \int_m^t \frac{n-\tau}{n-m} \cdot \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau. \\ &= u_2 + u_3'. \quad (m > t > n) \quad \dots \dots \dots (5) \end{aligned}$$

(4) after the surface temperature becomes zero at $t = n$, temperature at $t (> n)$ is given by

$$u_4 = \frac{kx}{2a\sqrt{\pi}} \int_0^m \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau + \frac{kx}{2a\sqrt{\pi}} \int_m^n \frac{n-\tau}{n-m} \cdot \frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} d\tau.$$

$$= u_2 + u_4' \quad (t > n) \quad \dots\dots\dots (6)$$

When we calculate the above each formula (3) ~ (6), we had better transform the variable and integrate

from $t - \tau = 0$ to $t - \tau = t$ in (3),

from $t - \tau = t - m$ to $t - \tau = t$ in (4),

from $t - \tau = 0$ to $t - \tau = t - m$ in (5),

from $t - \tau = t - \tau$ to $t - \tau = t - m$ in (6),

and about $\frac{n-\tau}{n-m}$ in (5), (6) calculate the value

$$\frac{n-\tau}{n-m} = \frac{n-t + (t-\tau)}{n-m} = r.$$

In this problem we assume that the substance is concrete

$$a^2 = 0.0064 \text{ (C.G.S. - unit)},$$

and we shall show the temperature change at 1.0 cm depth from the surface.

Then

$$\frac{x}{2a\sqrt{\pi}} = 3.52, \quad \frac{x^2}{4a^2} = 39.1$$

And the value of

$$\frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}} = \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$$

for various value of $t-\tau$ are shown as Table 1.

Relation of $t-\tau$ and $\frac{e^{-\frac{x^2}{4a^2(t-\tau)}}}{(t-\tau)^{\frac{3}{2}}}$ is illustrated in Fig. 2. It is showed from $t-\tau = 0$ till $t-\tau = 180$ in cases of $x = 0.5$ cm, 1.0 cm, and 1.5 cm.

When we calculate the integral value of (3) by the above, we can get the value of u_1 as Table 2.

This value u_1 is illustrated in Fig. 5 by thick full lines. In this diagram axis of abscissa shows the time t (sec.), and axis of ordinate shows the value of $\frac{u}{k}$. Then, we show the value of u_2 for various m by (4) in following Table 3. This value u_2 is illustrated in Fig. 5 by broken lines.

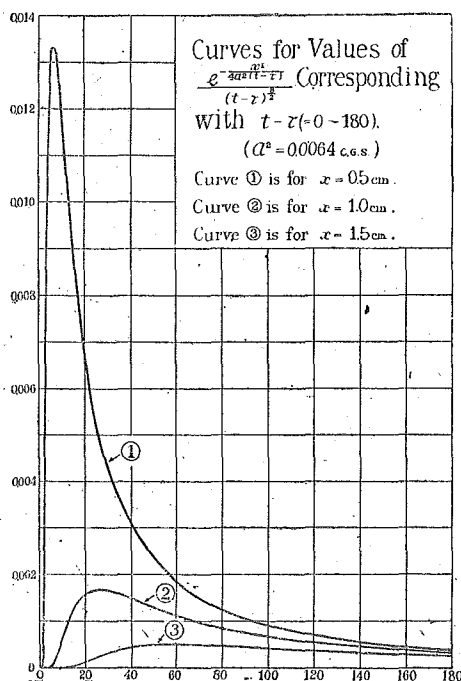


Fig. 2

Table 1.

$t-\tau$	$\frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	$t-\tau$	$\frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	$t-\tau$	$\frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	$t-\tau$	$\frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	$t-\tau$	$\frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$
0	0.	80	0.000856	1020	0.0000295	2100	0.0000102	3180	0.00000551
3	0.000000	100	0.000676	1080	0.0000272	2160	0.00000978	3200	0.00000545
4	0.000006	120	0.000548	1100	0.0000264	2200	0.00000952	3240	0.00000537
5	0.000036	140	0.000456	1140	0.0000251	2220	0.00000939	3300	0.00000521
6	0.000102	160	0.000386	1200	0.0000233	2280	0.00000903	3360	0.00000501
8	0.000331	180	0.000333	1260	0.0000217	2300	0.00000891	3400	0.00000498
10	0.000633	200	0.000290	1300	0.0000207	2340	0.00000869	3420	0.00000494
12	0.000922	240	0.000228	1320	0.0000202	2400	0.00000837	3480	0.00000482
14	0.001169	300	0.000169	1380	0.0000190	2460	0.00000807	3500	0.00000477
16	0.001361	360	0.000131	1400	0.0000185	2500	0.00000788	3540	0.00000470
18	0.001498	400	0.000113	1440	0.0000178	2520	0.00000778	3600	0.00000458
20	0.001575	420	0.000106	1500	0.0000168	2580	0.00000752	3800	0.00000423
22.5	0.001643	480	0.0000877	1560	0.0000158	2600	0.00000744	3900	0.00000407
25	0.001660	500	0.0000827	1600	0.0000153	2640	0.00000726	4000	0.00000391
27	0.001672	540	0.0000741	1620	0.0000150	2700	0.00000703	4200	0.00000364
28.5	0.001669	600	0.0000638	1680	0.0000142	2760	0.00000680	4500	0.00000328
30	0.001657	660	0.0000556	1700	0.0000140	2800	0.00000665	4800	0.00000299
32	0.001629	700	0.0000510	1740	0.0000135	2820	0.00000659	5100	0.00000273
34	0.001598	720	0.0000490	1800	0.0000128	2880	0.00000638	5400	0.00000250
36	0.001561	780	0.0000437	1860	0.0000122	2900	0.00000632	5600	0.00000238
38	0.001525	800	0.0000421	1900	0.0000118	2940	0.00000619	6000	0.00000214
40	0.001487	840	0.0000392	1920	0.0000116	3000	0.00000601	6400	0.00000194
44	0.001410	900	0.0000355	1980	0.0000111	3060	0.00000583	6600	0.00000185
50	0.001293	960	0.0000323	2000	0.0000110	3100	0.00000572	6800	0.00000177
60	0.001119	1000	0.0000304	2040	0.0000106	3120	0.00000567	7200	0.00000163

Table 2.

t	$\int_0^t \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_1	t	$\int_0^t \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_1	t	$\int_0^t \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_1
0	0.	0.	1500	0.2308	$k \times 0.813$	4200	0.2513	$k \times 0.884$
60	0.0704	$k \times 0.248$	1800	0.2352	" 0.829	4500	0.2523	" 0.888
120	0.1174	" 0.414	2100	0.2387	" 0.840	4800	0.2533	" 0.891
180	0.1430	" 0.504	2400	0.2414	" 0.850	5100	0.2541	" 0.894
240	0.1595	" 0.562	2700	0.2437	" 0.857	5400	0.2550	" 0.897
300	0.1713	" 0.604	3000	0.2457	" 0.865	6000	0.2563	" 0.902
600	0.2020	" 0.711	3300	0.2474	" 0.871	6600	0.2575	" 0.906
900	0.2163	" 0.762	3600	0.2488	" 0.876	7200	0.2585	" 0.910
1200	0.2250	" 0.793	3900	0.2501	" 0.880			

Table 3.

m	t	$t-m$	$\int_0^m \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_2	m	t	$t-m$	$\int_0^m \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_2
60	120	60	0.0470	$k \times 0.165$	600	3000	2700	0.0020	" 0.007
	180	120	0.0256	" 0.090		3300	3000	0.0017	" 0.006
	240	180	0.0165	" 0.058		3600	3300	0.0015	" 0.005
	300	240	0.0118	" 0.041		900	300	0.0455	$k \times 0.160$
	360	300	0.0091	" -0.032		1200	600	0.0229	" 0.081
	600	540	0.0041	" 0.015		1500	900	0.0146	" 0.051
	900	840	0.0022	" 0.008		1800	1200	0.0103	" 0.036
	1200	1140	0.0015	" 0.005		2100	1500	0.0078	" 0.028
120	180	60	0.0726	$k \times 0.256$	900	2400	1800	0.0062	" 0.022
	240	120	0.0421	" 0.148		2700	2100	0.0051	" 0.018
	300	180	0.0283	" 0.100		3000	2400	0.0043	" 0.015
	600	480	0.0090	" 0.032		960	60	0.1479	$k \times 0.521$
	900	780	0.0047	" 0.017		1080	180	0.0788	" 0.277
	1200	1080	0.0030	" 0.011		1200	300	0.0541	" 0.191
180	240	60	0.0890	$k \times 0.314$	1200	1500	600	0.0288	" 0.101
	300	120	0.0539	" 0.190		1800	900	0.0189	" 0.067
	360	180	0.0373	" 0.131		2100	1200	0.0138	" 0.048
	480	300	0.0222	" 0.078		2400	1500	0.0106	" 0.037
	600	420	0.0151	" 0.053		2700	1800	0.0085	" 0.030
	900	720	0.0076	" 0.027		3000	2100	0.0070	" 0.025
	1200	1020	0.0047	" 0.017		1500	300	0.0601	$k \times 0.211$
						1800	600	0.0332	" 0.117
240	300	60	0.1009	$k \times 0.355$	1500	2100	900	0.0224	" 0.079
	600	360	0.0222	" 0.078		2400	1200	0.0165	" 0.058
	900	660	0.0107	" 0.038		2700	1500	0.0129	" 0.045
	1200	960	0.0066	" 0.023		3000	1800	0.0105	" 0.037
300	360	60	0.1100	$k \times 0.387$	1800	1800	300	0.0645	$k \times 0.227$
	420	120	0.0702	" 0.247		2100	600	0.0367	" 0.129
	480	180	0.0505	" 0.178		2400	900	0.0252	" 0.089
	600	300	0.0312	" 0.110		2700	1200	0.0188	" 0.066
	900	600	0.0143	" 0.050	1800	3000	1500	0.0149	" 0.052
	1200	900	0.0086	" 0.030		1860	60	0.1656	$k \times 0.583$
	1500	1200	0.0059	" 0.021		1980	180	0.0939	" 0.331
	1800	1500	0.0044	" 0.015		2100	300	0.0679	" 0.239
	2100	1800	0.0034	" 0.012		2400	600	0.0394	" 0.139
	2400	2100	0.0028	" 0.010		2700	900	0.0275	" 0.097
	2700	2400	0.0023	" 0.008					

	3000	1200	0.0208	" 0.073		3900	1200	0.0251	" 0.089
	3300	1500	0.0165	" 0.058	2700	4200	1500	0.0205	" 0.072
	3600	1800	0.0136	" 0.048		4500	1800	0.0171	" 0.061
	3900	2100	0.0114	" 0.040		4800	2100	0.0146	" 0.051
	4200	2400	0.0099	" 0.035		5400	2700	0.0113	" 0.039
	4500	2700	0.0086	" 0.021		6000	3300	0.0089	" 0.031
	5400	3600	0.0062	" 0.020		7200	4500	0.0062	" 0.022
2100	2400	300	0.0707	$k \times 0.249$	3000	3300	300	0.0766	$k \times 0.270$
	2700	600	0.0417	" 0.147		3600	600	0.0468	" 0.165
	3000	900	0.0294	" 0.103	3300	3600	300	0.0781	$k \times 0.275$
	3300	1200	0.0225	" 0.079	3600	3660	60	0.1787	$k \times 0.629$
	3600	1500	0.0180	" 0.063		3780	180	0.1066	" 0.375
2400	2700	300	0.0730	$k \times 0.257$		3900	300	0.0788	" 0.277
	3000	600	0.0437	" 0.154		4200	600	0.0493	" 0.173
	3300	900	0.0311	" 0.109		4500	900	0.0360	" 0.127
	3600	1200	0.0240	" 0.084		4800	1200	0.0284	" 0.100
						5100	1500	0.0233	" 0.082
	2760	60	0.1737	$k \times 0.611$		5400	1800	0.0200	" 0.069
	2880	180	0.1019	" 0.359		6000	2400	0.0149	" 0.052
	3000	300	0.0749	" 0.264		6600	3000	0.0118	" 0.042
	3300	600	0.0454	" 0.160		7200	3600	0.0097	" 0.034
	3600	900	0.0325	" 0.115					

Next, for determining u_3 and u_4 by (5) and (6), we assume the following values of m and n :

$$\begin{array}{llll}
 m=60, & n=180; & m=300, & n=600; \\
 m=60, & n=360; & m=900, & n=1200; \\
 m=180, & n=360; & m=900, & n=1800; \\
 m=180, & n=480; & m=1800, & n=2100; \\
 m=300, & n=420; & m=1800, & n=2700;
 \end{array}
 \quad
 \begin{array}{llll}
 m=1800, & n=3600; & m=3600, & n=3900; \\
 m=2700, & n=3000; & m=3600, & n=4500; \\
 m=2700, & n=3600; & m=3600, & n=5400; \\
 m=2700, & n=4500; & m=3600, & n=7200.
 \end{array}$$

Now, as the preparation of obtaining the integration of u_3' in (5) we must decide the value of

$$\frac{n-\tau}{n-m} \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} = r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$$

corresponding to the various value of $t-\tau$. As one example, we show that value at $t=240, 300$, and 360 in cases of $m=180$ and $n=360$. It is shown in the table 4. In this case the relation between $t-\tau$ and

$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$ is represented by the curves is Fig. 3, and then we shall be able to require the integral of u_3' .

Similarly, we must decide the value of

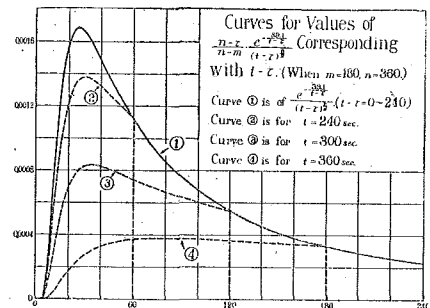


Fig. 3.

$$\frac{n-m}{n-m} \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} = r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$$

for u_4' . As before, temperatures at $t=480, 600, 900, 1800$ and 2700 in cases of $m=180$ and $n=360$ are shown in Table 5.

In this case the relation between $t-\tau$ and $r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$ is illustrated by the curves in Fig. 4, then we shall be able to obtain the integral of u_4' .

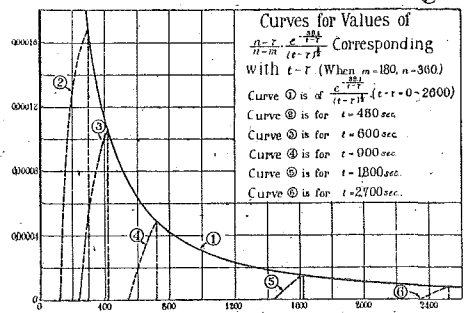


Fig. 4.

Thus by obtaining the integrals for the various time t for a certain m and n , the values of u_3' and u_4' will be calculated and finally u_3 and u_4 . It is as shown in Table 6. This results is illustrated by Fig. 5, by fine full lines. In the same way the results are illustrated by Fig. 6, 7 and 8 for $x=2$ cm, 3 cm, and 4 cm respectively.

Table 4.

$m=180, \quad n=360, \quad n-m=180$						
$t-\tau$	$t=240, t-m=60, r=\frac{120+(t-\tau)}{180}$		$t=300, t-m=120, r=\frac{60+(t-\tau)}{180}$		$t=360, t-m=180, r=\frac{t-\tau}{180}$	
	r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$	r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$
0	0.6667	0.	0.3333	0.	0.	0.
3	0.6833	0.000000	0.3500	0.000000	0.0167	0.000000
4	0.6889	0.000004	0.3556	0.000002	0.0222	0.000000
5	0.6944	0.000025	0.3611	0.000012	0.0278	0.000001
6	0.7000	0.000071	0.3667	0.000037	0.0333	0.000003
8	0.7111	0.000235	0.3778	0.000125	0.0444	0.000015
10	0.7222	0.000457	0.3889	0.000246	0.0556	0.000035
12	0.7333	0.000676	0.4000	0.000369	0.0667	0.000061
14	0.7444	0.000870	0.4111	0.000481	0.0778	0.000091
16	0.7556	0.001028	0.4222	0.000575	0.0889	0.000121
18	0.7667	0.001148	0.4333	0.000649	0.1000	0.000150
20	0.7778	0.001225	0.4444	0.000700	0.1111	0.000175
22.5	0.7917	0.001301	0.4583	0.000753	0.1250	0.000205
25	0.8056	0.001354	0.4722	0.000794	0.1389	0.000233
27	0.8167	0.001365	0.4833	0.000808	0.1500	0.000251
28.5	0.8250	0.001377	0.4917	0.000821	0.1583	0.000264
30	0.8333	0.001381	0.5000	0.000829	0.1667	0.000276
32	0.8444	0.001376	0.5111	0.000833	0.1778	0.000290
34	0.8556	0.001367	0.5222	0.000835	0.1889	0.000302
36	0.8667	0.001353	0.5333	0.000833	0.2000	0.000312
38	0.8778	0.001339	0.5444	0.000830	0.2111	0.000322
40	0.8889	0.001322	0.5556	0.000826	0.2222	0.000330
50	0.9444	0.001221	0.6111	0.000790	0.2778	0.000359
60	1.0000	0.001119	0.6667	0.000746	0.3333	0.000373
80			0.7778	0.000666	0.4444	0.000380
100			0.8889	0.000601	0.5556	0.000376
120			1.0000	0.000548	0.6667	0.000365
140					0.7778	0.000355
160					0.8889	0.000343
180					1.0000	0.000333

Table 5.

$m = 180, \quad n = 360, \quad n-m = 180$								
$t-\tau$	$t=480, t-m=300, r=\frac{(t-\tau)-120}{180}$		$t-\tau$	$t=600, t-m=420, r=\frac{(t-\tau)-240}{180}$		$t-\tau$	$t=900, t-m=720, r=\frac{(t-\tau)-540}{180}$	
	r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$		r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$		r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$
120	0.	0.	240	0.	0.	540	0.	0.
140	0.1111	0.000051	300	0.3333	0.000056	600	0.3333	0.000021
160	0.2222	0.000086	400	0.8889	0.000101	700	0.8889	0.000045
180	0.3333	0.000111	420	1.0000	0.000106	720	1.0000	0.000049
200	0.4444	0.000129						
240	0.6667	0.000152						
300	1.0000	0.000169						

$t-\tau$	$t=1800, t-m=1620, r=\frac{(t-\tau)-1440}{180}$		$t-\tau$	$t=2700, t-m=2520, r=\frac{(t-\tau)-2340}{180}$	
	r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$		r	$r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}}$
1440	0.	0.	2340	0.	0.
1500	0.3333	0.000006	2400	0.3333	0.000003
1600	0.8889	0.000014	2500	0.8889	0.000007
1620	1.0000	0.000015	2520	1.0000	0.000008

Table 6.

m	n	t	$\int_m^t r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_3'	u_3	$\int_m^n r \cdot \frac{e^{-\frac{39.1}{t-\tau}}}{(t-\tau)^{\frac{3}{2}}} d\tau$	u_4'	u_4
60	180	120	0.0563	$k \times 0.198$	$k \times 0.364$			
		180	0.0542	" 0.191	" 0.281			
		240				0.0289	$k \times 0.102$	$k \times 0.160$
		300				0.0179	" 0.063	" 0.104
		600				0.0048	" 0.017	" 0.031
		900				0.0025	" 0.009	" 0.017
	360	120	0.0657	$k \times 0.231$	$k \times 0.400$			
		180	0.0930	" 0.328	" 0.418			
		240	0.0920	" 0.324	" 0.382			
		300	0.0779	" 0.274	" 0.316			
		360	0.0562	" 0.198	" 0.230			
		600				0.0155	$k \times 0.055$	$k \times 0.069$
		900				0.0072	" 0.025	" 0.033

180	360	240	0.0615	$k \times 0.217$	$k \times 0.530$			
		300	0.0758	" 0.267	" 0.456			
		360	0.0571	" 0.201	" 0.332			
		480				0.0216	$k \times 0.076$	$k \times 0.154$
		600				0.0116	" 0.041	" 0.094
		900				0.0049	" 0.017	" 0.044
	480	240	0.0657	$k \times 0.231$	$k \times 0.545$			
		300	0.0860	" 0.327	" 0.517			
		480	0.0562	" 0.198	" 0.276			
		600				0.0254	$k \times 0.089$	$k \times 0.143$
		900				0.0092	" 0.032	" 0.059
300	420	360	0.0563	$k \times 0.198$	$k \times 0.586$			
		420	0.0542	" 0.191	" 0.438			
		480				0.0289	$k \times 0.102$	$k \times 0.279$
		600				0.0122	" 0.043	" 0.153
		900				0.0040	" 0.014	" 0.064
		1800				0.0010	" 0.004	" 0.019
	600	360	0.0657	$k \times 0.231$	$k \times 0.618$			
		480	0.0920	" 0.324	" 0.501			
		600	0.0562	" 0.198	" 0.308			
		900				0.0128	$k \times 0.045$	$k \times 0.095$
		1200				0.0064	" 0.023	" 0.053
		1800				0.0028	" 0.010	" 0.025
		2700				0.0013	" 0.005	" 0.013
900	1200	960	0.0657	$k \times 0.231$	$k \times 0.752$			
		1080	0.0920	" 0.324	" 0.601			
		1200	0.0562	" 0.198	" 0.388			
		1500				0.0128	$k \times 0.045$	$k \times 0.147$
		1800				0.0064	" 0.023	" 0.089
		2700				0.0021	" 0.007	" 0.037
	1800	1200	0.1367	$k \times 0.481$	$k \times 0.672$			
		1500	0.1009	" 0.355	" 0.457			
		1800	0.0449	" 0.158	" 0.198			
		2100				0.0182	$k \times 0.064$	$k \times 0.113$
		2700				0.0079	" 0.028	" 0.058
		3600				0.0038	" 0.013	" 0.031
		1860	0.0657	$k \times 0.231$	$k \times 0.814$			
		1980	0.0920	" 0.324	" 0.654			
		2100	0.0562	" 0.198	" 0.437			

1800	2100	2400				0.0128	$k \times 0.045$	$k \times 0.184$
		2700				0.0064	" 0.023	" 0.119
		3600				0.0021	" 0.007	" 0.055
	2700	2100	0.1367	$k \times 0.481$	$k \times 0.720$			
		2400	0.1009	" 0.355	" 0.494			
		2700	0.0449	" 0.158	" 0.255			
		3000				0.0182	$k \times 0.064$	$k \times 0.137$
		3600				0.0079	" 0.028	" 0.076
		4500				0.0038	" 0.013	" 0.035
	3600	2100	0.1544	$k \times 0.543$	$k \times 0.782$			
		2400	0.1525	" 0.537	" 0.675			
		2700	0.1313	" 0.462	" 0.559			
		3000	0.1031	" 0.363	" 0.436			
		3300	0.0702	" 0.247	" 0.305			
		3600	0.0359	" 0.126	" 0.174			
		3900				0.0189	$k \times 0.067$	$k \times 0.107$
		4200				0.0133	" 0.047	" 0.081
		5400				0.0056	" 0.020	" 0.040
	3000	2760	0.0657	$k \times 0.231$	$k \times 0.843$			
		2880	0.0920	" 0.324	" 0.681			
		3000	0.0562	" 0.198	" 0.462			
		3300				0.0128	$k \times 0.045$	$k \times 0.205$
		3600				0.0064	" 0.023	" 0.138
		4500				0.0021	" 0.007	" 0.038
2700	3600	3000	0.1367	$k \times 0.481$	$k \times 0.745$			
		3300	0.1009	" 0.355	" 0.515			
		3600	0.0449	" 0.158	" 0.273			
		3900				0.0182	$k \times 0.064$	$k \times 0.153$
		4200				0.0112	" 0.039	" 0.111
		5400				0.0038	" 0.013	" 0.053
	4500	3000	0.1544	$k \times 0.543$	$k \times 0.807$			
		3300	0.1525	" 0.537	" 0.696			
		3600	0.1313	" 0.462	" 0.577			
		3900	0.1031	" 0.363	" 0.452			
		4200	0.0702	" 0.247	" 0.319			
		4500	0.0359	" 0.126	" 0.186			
		4800				0.0189	$k \times 0.067$	$k \times 0.118$
		5400				0.0101	" 0.036	" 0.075
		6000				0.0067	" 0.024	" 0.055

5400	3000	0.1599	$k \times 0.563$	$k \times 0.827$			
	3300	0.1696	" 0.597	" 0.757			
	3600	0.1608	" 0.566	" 0.681			
	4200	0.1246	" 0.439	" 0.511			
	4800	0.0799	" 0.281	" 0.332			
	5400	0.0307	" 0.108	" 0.147			
	6000				0.0137	$k \times 0.048$	$k \times 0.079$
	7200				0.0066	" 0.023	" 0.045
3600	3900	3660	0.0657	$k \times 0.221$	$k \times 0.850$		
		3780	0.0920	" 0.324	" 0.699		
		3900	0.0562	" 0.198	" 0.475		
		4200				0.0128	$k \times 0.045$
		4500				0.0064	" 0.023
		5400				0.0021	" 0.007
	4500	3900	0.1367	$k \times 0.481$	$k \times 0.759$		
		4200	0.1009	" 0.355	" 0.529		
		4500	0.0449	" 0.158	" 0.285		
		4800				0.0182	$k \times 0.064$
		5400				0.0079	" 0.038
		6000				0.0047	" 0.016
	5400	3900	0.1544	$k \times 0.543$	$k \times 0.821$		
		4200	0.1525	" 0.537	" 0.710		
		4500	0.1313	" 0.462	" 0.589		
		4800	0.1031	" 0.363	" 0.463		
		5100	0.0702	" 0.247	" 0.329		
		5400	0.0359	" 0.126	" 0.196		
		6000				0.0133	$k \times 0.047$
		7200				0.0056	" 0.020
	7200	3900	0.1632	$k \times 0.574$	$k \times 0.852$		
		4200	0.1780	" 0.627	" 0.800		
		4800	0.1648	" 0.580	" 0.680		
		5400	0.1361	" 0.479	" 0.548		
		6000	0.1022	" 0.360	" 0.412		
		6600	0.0704	" 0.231	" 0.272		
		7200	0.0280	" 0.097	" 0.133		

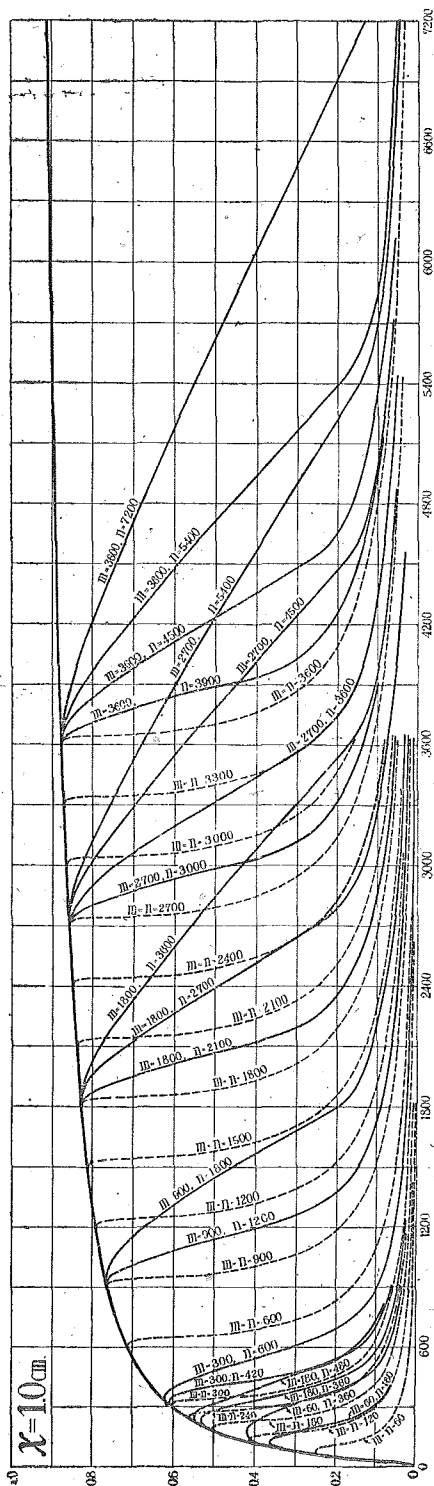


Fig. 5

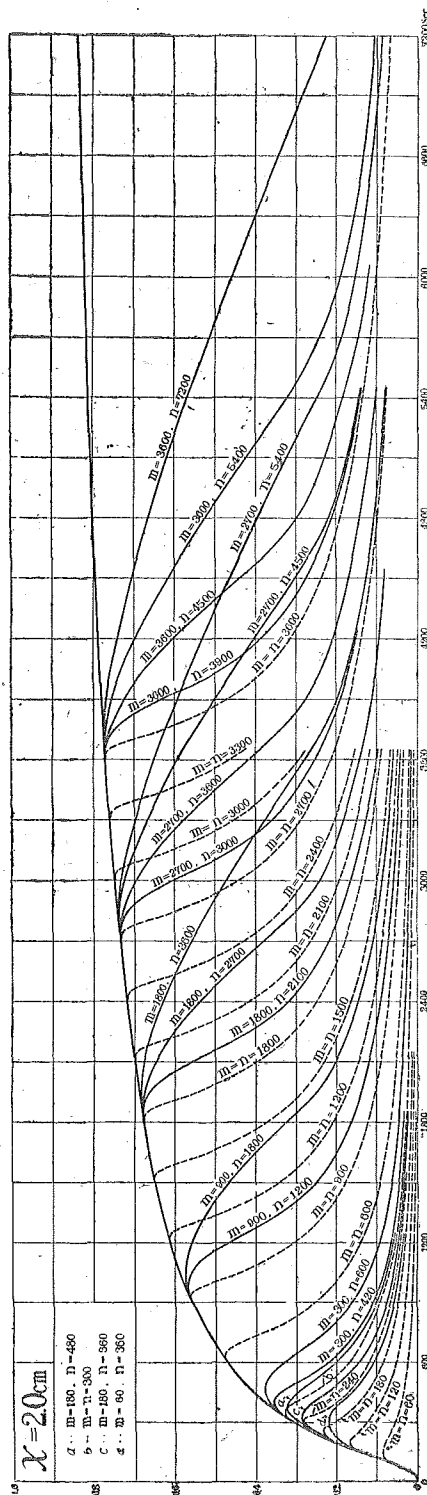


Fig. 6

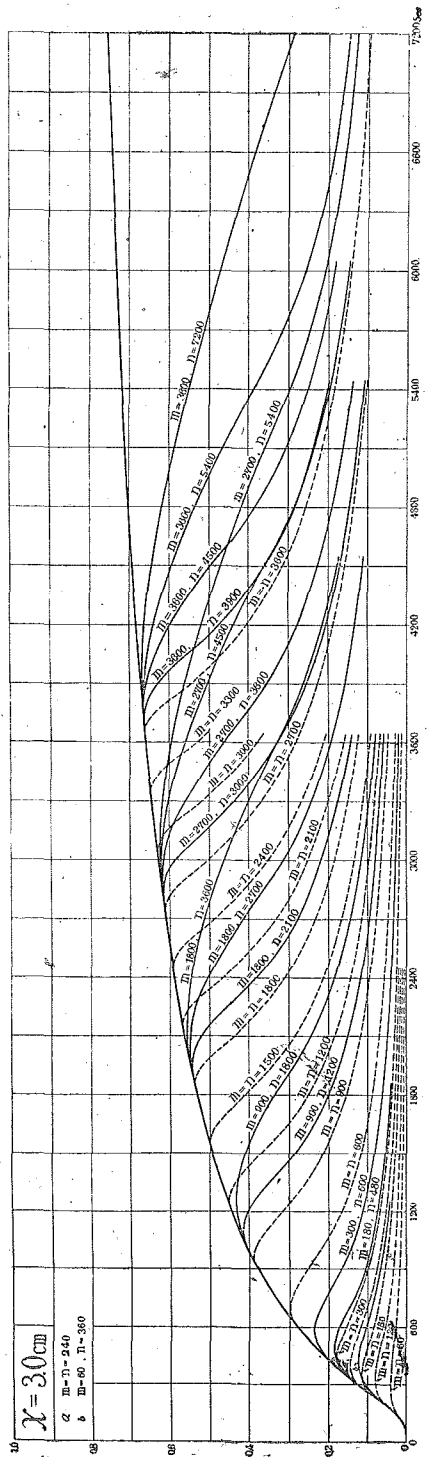


Fig. 7

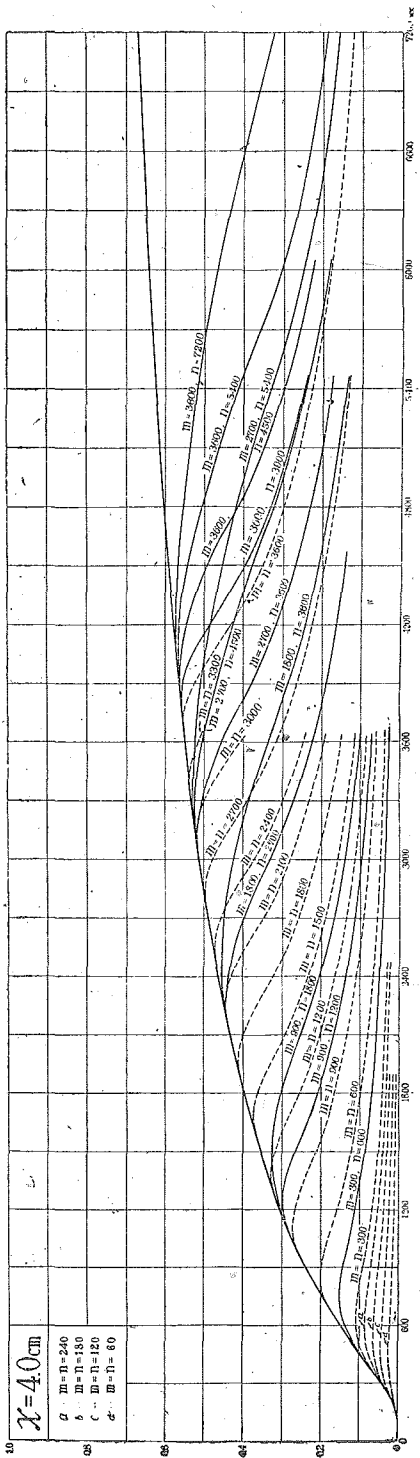


Fig. 8

3. Heat Conduction of the Solid Bounded by two Parallel Planes.

In this paragraph the temperature distribution is calculated when the range of x is limited to the interval $0 \leq x \leq C$. Let the solid be bounded by the planes $x=0$ and $x=C$, initial temperature being given by $u=0$, and surface temperature varying with the time, and back plane $x=C$ being thermally insulated. In this plate, where u has to satisfy

$$\frac{\partial u}{\partial t} = a^2 \frac{\partial^2 u}{\partial x^2}, \dots\dots\dots (7)$$

$$\left. \begin{array}{lll} u=0 & \text{when} & t=0, \\ u=f(t) & \text{at} & x=0, \\ \frac{\partial u}{\partial x}=0 & \text{at} & x=C, \end{array} \right\}$$

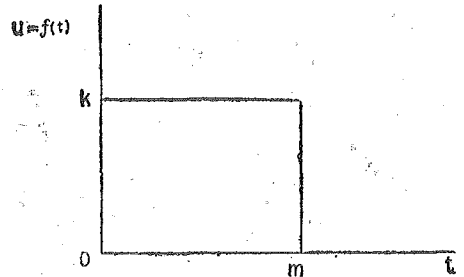


Fig. 9

the solution is given by

$$u = \frac{2}{C} \sum_{n=0}^{\infty} \sin \frac{2n+1}{2C} \pi x \frac{a^2(2n+1)\pi}{C} \int_0^t f(\tau) e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 (t-\tau)} d\tau \dots\dots\dots (8)$$

Now, especially the temperature change at the thermally insulated back plane $x=C$ alone will be calculated numerically. It follows from (8)

$$u = \frac{2a^2}{C} \sum_{n=0}^{\infty} (-1)^n \frac{2n+1}{2C} \pi \int_0^t f(\tau) e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 (t-\tau)} d\tau \dots\dots\dots (9)$$

As the last paragraph let the temperature $u=f(t)$ at $x=0$ be in such a state that steady temperature continues a certain duration, then it breaks off as shown by Fig. 9,

$$f(t) = k \quad \text{between} \quad t=0 \quad \text{and} \quad t=m,$$

$$\text{and} \quad f(t) = 0 \quad \text{when} \quad t > m.$$

Then we shall be able to think the following two cases:

(1) when $t < m$, from (9) it follows that

$$\begin{aligned} u_1 &= \frac{2k}{C} \sum_{n=0}^{\infty} (-1)^n \frac{2n+1}{2C} \pi a^2 \frac{1}{a^2 \left(\frac{2n+1}{2C} \pi \right)^2} \left[e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 (t-\tau)} \right]_0^t \\ &= k \left\{ 1 - \frac{4}{\pi} \sum_{n=0}^{\infty} \frac{(-1)^n}{2n+1} e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 t} \right\} \dots\dots\dots (10) \end{aligned}$$

(2) when $t > m$, from (9) it follows that

$$u_2 = \frac{4k}{\pi} \sum_{n=0}^{\infty} \frac{(-1)^n}{2n+1} \left\{ e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 (t-m)} - e^{-a^2 \left(\frac{2n+1}{2C} \pi \right)^2 t} \right\} \dots\dots\dots (11)$$

Writing $b = \frac{a^2 \pi^2}{4C^2}$ and expanding (10) and (11), it follows that

$$u_1 = k \left[1 - \frac{4}{\pi} \left(e^{-bt} - \frac{1}{3} e^{-9bt} + \frac{1}{5} e^{-25bt} - \frac{1}{7} e^{-49bt} + \frac{1}{9} e^{-81bt} - \dots \right) \right] (t < m), \quad \dots (12)$$

and
$$u_2 = \frac{4k}{\pi} \left[\left(e^{-b(t-m)} - \frac{1}{3} e^{-9b(t-m)} + \dots \right) - \left(e^{-bt} - \frac{1}{3} e^{-9bt} + \dots \right) \right] (t > m). \quad \dots (13)$$

In the above formulae when t is large enough, we may neglect the quantity under $\frac{1}{3} e^{-9bt}$.

Also in this problem, we assume $a^2 = 0.0064$ (C.G.S.—unit), and we shall show the temperature change at $C = 4.0$ cm. Then we get $b = 0.000987$.

Therefore as the values of u for the various t , we obtain the Table 7, from (12).

These values of u are illustrated in Fig. 10 by full line. In this diagram the axis of abscissa shows the time t (sec.) and the axis of ordinate shows the value of $\frac{u}{k}$.

When we require the values of u_2 for various t and m from (13), we can directly apply Table 7. Therefore we obtain the Table 8.

Table 7.

t	e^{-bt}	$-\frac{1}{3} e^{-9bt}$	$\frac{1}{5} e^{-25bt}$	$-\frac{1}{7} e^{-49bt}$	$\frac{1}{9} e^{-81bt}$
0					
60	0.9425	- 0.1956	0.0455	- 0.0078	- 0.0009
120	0.8883	- 0.1148	0.0102	- 0.0004	0.0000
300	0.7437	- 0.0232	0.0001	- 0.0000	—
360	0.7010	- 0.0136	0.0000	—	—
420	0.6607	- 0.0080	—	—	—
600	0.5531	- 0.0016	—	—	—
660	0.5213	- 0.0009	—	—	—
720	0.4913	- 0.0006	—	—	—

$\sum_{n=0}^{\infty} \frac{(-1)^n e^{-(2n+1)^2 bt}}{2n+1}$	$\frac{4}{\pi} \sum_{n=0}^{\infty} \frac{(-1)^n e^{-(2n+1)^2 bt}}{2n+1}$	u_1
	1.	$k \times 0.$
0.7854	1.000	" 0.000
0.7833	0.997	" 0.003
0.7206	0.918	" 0.082
0.6874	0.875	" 0.125
0.6527	0.831	" 0.169
0.5515	0.702	" 0.298
0.5204	0.663	" 0.337
0.4908	0.625	" 0.375

t	e^{-bt}	$\frac{4}{\pi} e^{-bt}$	u_1	t	e^{-bt}	$\frac{4}{\pi} e^{-bt}$	u_1	t	e^{-bt}	$\frac{4}{\pi} e^{-bt}$	u_1
900	0.4114	0.524	$k \times 0.476$	2400	0.0936	0.119	$k \times 0.881$	3900	0.0213	0.027	$k \times 0.973$
960	0.3877	0.494	" 0.506	2460	0.0882	0.112	" 0.888	4200	0.0158	0.020	" 0.980
1020	0.3654	0.465	" 0.535	2520	0.0832	0.106	" 0.894	4500	0.0118	0.015	" 0.985
1200	0.3060	0.390	" 0.610	2700	0.0696	0.089	" 0.911	4800	0.0088	0.011	" 0.989
1260	0.2884	0.367	" 0.633	2760	0.0656	0.084	" 0.916	5100	0.0065	0.008	" 0.992
1320	0.2718	0.346	" 0.654	2820	0.0618	0.079	" 0.921	5400	0.0049	0.006	" 0.994
1500	0.2275	0.290	" 0.710	3000	0.0514	0.065	" 0.935	5460	0.0046	0.006	" 0.994
1560	0.2145	0.273	" 0.727	3060	0.0488	0.062	" 0.938	5520	0.0043	0.005	" 0.995
1620	0.2021	0.257	" 0.743	3120	0.0460	0.059	" 0.941	5700	0.0036	0.005	" 0.995
1800	0.1692	0.215	" 0.785	3200	0.0385	0.049	" 0.951	6000	0.0027	0.003	" 0.997
1860	0.1595	0.203	" 0.797	3360	0.0363	0.046	" 0.954	6300	0.0020	0.003	" 0.997
1920	0.1503	0.191	" 0.809	3420	0.0342	0.044	" 0.956	6600	0.0015	0.002	" 0.998
2100	0.1259	0.160	" 0.840	3600	0.0286	0.036	" 0.964	6900	0.0011	0.001	" 0.999
2160	0.1186	0.151	" 0.849	3660	0.0270	0.034	" 0.966	7200	0.0008	0.001	" 0.999
2220	0.1118	0.142	" 0.858	3720	0.0254	0.032	" 0.968				

Table 8.

m	t	$t-m$	u_2	m	t	$t-m$	u_2	m	t	$t-m$	u_2
300	360	60	$k \times 0.125$	900	2700	2100	" 0.072	1200	1620	420	" 0.574
	420	120	" 0.166		3000	2400	" 0.054		1800	600	" 0.487
	600	300	" 0.215		3300	2700	" 0.040		2100	900	" 0.363
	660	360	" 0.213		960	60	$k \times 0.506$		2400	1200	" 0.270
	900	600	" 0.179		1020	120	" 0.532		2700	1500	" 0.201
	1200	900	" 0.134		1200	300	" 0.528		3000	1800	" 0.150
	1500	1200	" 0.100		1500	600	" 0.412		3300	2100	" 0.111
	1800	1500	" 0.074		1800	900	" 0.308		3600	2400	" 0.083
	2100	1800	" 0.055		2100	1200	" 0.229		3900	2700	" 0.062
	2400	2100	" 0.041		2400	1500	" 0.171		4200	3000	" 0.045
600	660	60	$k \times 0.337$	1500	2700	1800	" 0.127	1500	1560	60	$k \times 0.727$
	720	120	" 0.372		3000	2100	" 0.095		1620	120	" 0.740
	900	300	" 0.394		3300	2400	" 0.070		1800	300	" 0.702
	960	360	" 0.382		3600	2700	" 0.052		1920	420	" 0.640
	1200	600	" 0.313		3900	3000	" 0.038		2100	600	" 0.542
	1500	900	" 0.234		1260	60	$k \times 0.633$		2400	900	" 0.403
	1800	1200	" 0.174		1320	120	" 0.651		2700	1200	" 0.301
	2100	1500	" 0.129		1500	300	" 0.628		3000	1500	" 0.224
	2400	1800	" 0.096						3300	1800	" 0.166

	3600	2100	" 0.124		5700	3300	" 0.044		3660	60	$k \times 0.966$
	3900	2400	" 0.092		2760	60	$k \times 0.916$		3720	120	" 0.965
	4200	2700	" 0.068		2820	120	" 0.919		3900	300	" 0.890
	4500	3000	" 0.050		3000	360	" 0.852		4200	600	" 0.682
1800	1860	60	$k \times 0.797$	2700	3120	420	" 0.772	3600	4500	900	" 0.509
	1920	120	" 0.806		3300	600	" 0.673		4800	1200	" 0.378
	2100	300	" 0.757		3420	720	" 0.581		5100	1500	" 0.281
	2220	420	" 0.689		3600	900	" 0.487		5400	1800	" 0.209
	2400	600	" 0.583		3900	1200	" 0.362		5700	2100	" 0.156
	2700	900	" 0.435		4200	1500	" 0.270		6000	2400	" 0.116
	3000	1200	" 0.324		4500	1800	" 0.200		6300	2700	" 0.086
	3300	1500	" 0.241		4800	2100	" 0.149		6600	3000	" 0.064
	3600	1800	" 0.179		5100	2400	" 0.111		6900	3300	" 0.048
	3900	2100	" 0.133		5400	2700	" 0.082	4200	4500	300	$k \times 0.903$
	4200	2400	" 0.099		5700	3000	" 0.061		4800	600	" 0.691
	4500	2700	" 0.074		6000	3300	" 0.046		5100	900	" 0.515
2100	4800	3000	" 0.054	3000	3060	60	$k \times 0.938$		5400	1200	" 0.384
	5100	3300	" 0.041		3120	120	" 0.939		5700	1500	" 0.285
	2160	60	$k \times 0.849$		3300	300	" 0.869		6600	1800	" 0.212
	2220	120	" 0.855		3420	420	" 0.787		6300	2100	" 0.168
	2400	300	" 0.798		3600	600	" 0.666		6600	2400	" 0.117
	2520	420	" 0.725		3720	720	" 0.592		6000	2700	" 0.087
	2700	600	" 0.614		3900	900	" 0.497		7200	3000	" 0.064
	3000	900	" 0.458		4290	1200	" 0.369	4800	5100	300	$k \times 0.909$
	3360	1200	" 0.341		4500	1500	" 0.275		5400	600	" 0.696
	3600	1500	" 0.253		4800	1800	" 0.204		5700	900	" 0.519
	3900	1800	" 0.188		5100	2100	" 0.152		6000	1200	" 0.386
	4200	2100	" 0.140		5400	2400	" 0.113		6200	1500	" 0.287
	4500	2400	" 0.104		5700	2700	" 0.084		6600	1800	" 0.214
	4800	2700	" 0.077		6000	3000	" 0.062		6900	2100	" 0.159
	5100	3000	" 0.057		6300	3300	" 0.046		7200	2400	" 0.118
2400	5400	3300	" 0.043	3300	3360	60	$k \times 0.954$	5400	5460	60	$k \times 0.994$
	2460	60	$k \times 0.888$		3420	120	" 0.954		5520	120	" 0.992
	2520	120	" 0.891		3600	300	" 0.881		5700	300	" 0.913
	2700	300	" 0.829		3720	420	" 0.798		6000	600	" 0.699
	2820	420	" 0.752		3900	600	" 0.675		6300	900	" 0.521
	3000	600	" 0.637		4200	900	" 0.503		6600	1200	" 0.388
	3300	900	" 0.475		4500	1200	" 0.375		6900	1500	" 0.288
	3600	1200	" 0.353		4800	1500	" 0.279		7200	1800	" 0.214
	3900	1500	" 0.263		5100	1800	" 0.207	6000	6300	300	$k \times 0.915$
	4200	1800	" 0.195		5400	2100	" 0.154		6600	600	" 0.700
	4500	2100	" 0.145		5700	2400	" 0.115		6900	900	" 0.522
	4800	2400	" 0.108		6000	2700	" 0.085		7200	1200	" 0.389
	5100	2700	" 0.080		6300	3000	" 0.063				
	5400	3000	" 0.059		6600	3300	" 0.047				

These values of u are illustrated in Fig. 10 by broken lines.

In the same way the result of calculation for $C = 10.0$ cm is illustrated by Fig. 11.

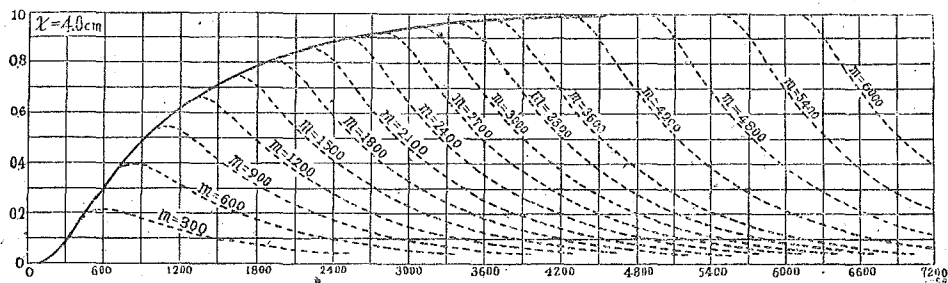


Fig. 10.

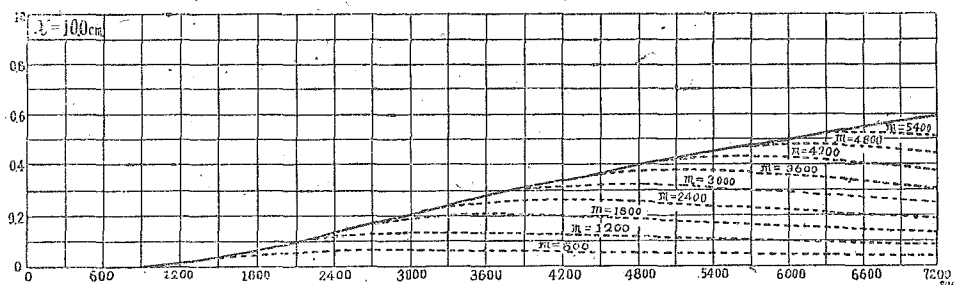


Fig. 11 (a).

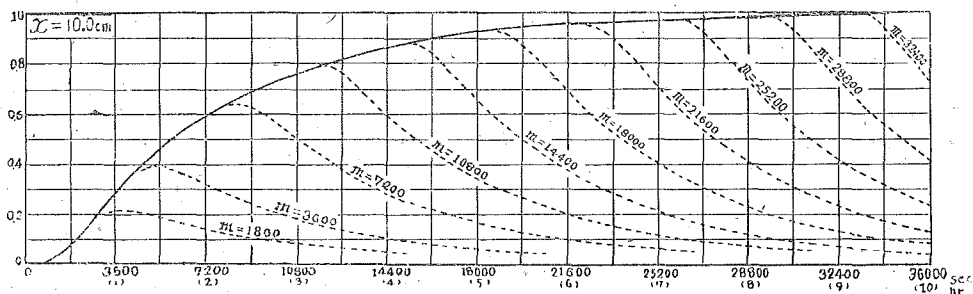


Fig. 11 (b).

4. Application.

Now we shall show the similarity of heat conduction between the geometrically similar two solids. Let the two similar solids have the relation as Table 9., and let $\varphi = \frac{l_1}{l_2}$ be the dimension ratio, $\varrho = \frac{u_1}{u_2}$ be the temperature ratio, and $\delta = \frac{t_1}{t_2}$ be the time ratio. As the above examples we think about the direction of x -axis. Then the differential equations of the heat conduction are respectively as follows

Table 9.

	Solid I.	Solid II.
Diffusivity	a_1^2	a_2^2
Dimension	l_1	l_2
Temperature	u_1	u_2
Time	t_1	t_2

$$\frac{\partial u_1}{\partial t_1} = a_1^2 \frac{\partial^2 u_1}{\partial x_1^2}, \quad \dots\dots\dots (14)$$

$$\frac{\partial u_2}{\partial t_2} = a_2^2 \frac{\partial^2 u_2}{\partial x_2^2}. \quad \dots\dots\dots (15)$$

In the case of similar state, we obtain

$$\frac{\theta}{\delta} = \frac{a_1^2}{a_2^2} \cdot \frac{\theta}{\varphi^2}$$

$$\text{or } \delta = \varphi^2 \frac{a_2^2}{a_1^2} \quad \dots\dots\dots (16)$$

from (14) and (15).

According to (16), if the relation between temperature and time about certain dimension l_1 for the material having the diffusivity a_1^2 is given, we shall be able to obtain the relation about any dimension l_2 for other material having the diffusivity a_2^2 .

Accordingly, in conformity with above examples of calculation in paragraph 2 and 3, we can apply the similarity of heat conduction to the various problems.

And then in the above two paragraphs we have shown the state of heat conduction in the semi-infinite solid and the solid plate. We shall be able to think that the temperature distribution in the most cases may be looked upon as the one in the intermediate case of these two extreme cases. Therefore the state of temperature distribution and change for the real substance can be estimated roughly from above two calculations.

At the end of this treatise I express my sense of gratitude to Prof. Y. Ikeda and Prof. K. Otubo.